

Aureenne Mining

Mt Ida Gold Project

STAGE 1 WORKS APPROVAL

Process Plant

Environmental Compliance Report

PROCESSING INFRASTRUCTURE

M 29/150, M 29/151, G 29/29, G 29/30,

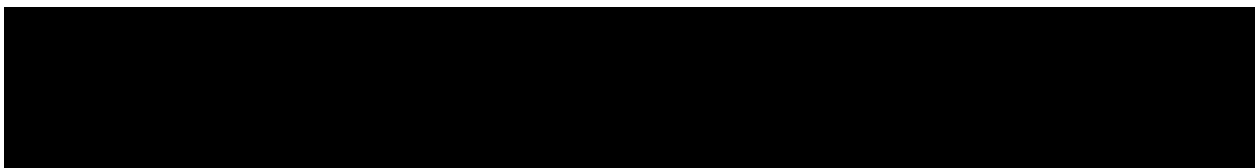
L 29/143, L 29/153, L 29/154, L 29/137, E 29/1007

July 2023

Aurenne Mining

Level 1, 10 Ord Street West Perth, WA 6005

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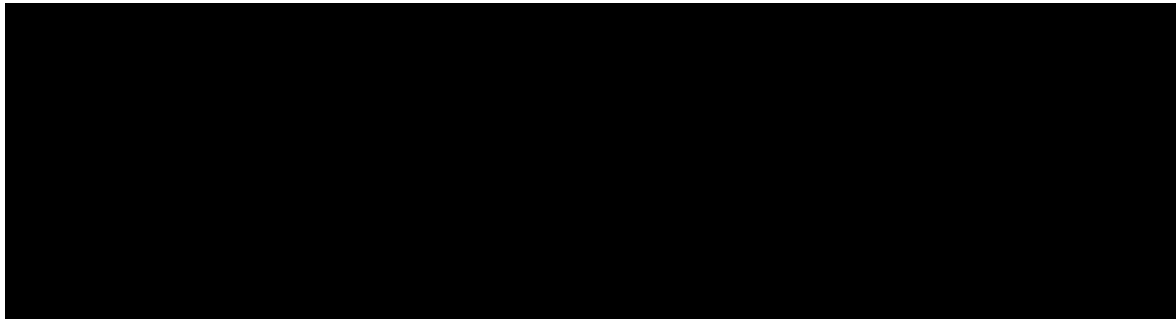


THE AURENNE GROUP OF COMPANIES
A Mining and Exploration Enterprise.

ENVIRONMENTAL COMPLIANCE REPORT PROCESS PLANT

For and on behalf of Aurenne MIT Pty Ltd I, Peter Story being a duly authorised person of the above company hereby confirm that the Process Plant and its associated infrastructure being chemical storage, diesel , raw water and process water storage , approximately 100 km northwest of Menzies in Western Australia, has been constructed in general accordance to the requirements of Works Approval 6640/2022/1 namely Conditions 5 , 10 and 11.

Name of authorised person



For and on behalf of Aurenne MIT Pty Ltd

Date:

15 July 2023.

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	<p align="center">STAGE 1 WORKS APPROVAL – CRITICAL CONSTRUCTION INFRASTRUCTURE REPORT IWL TSF</p> <p align="center">MINE PROCESSING & SUPPORTING INFRASTRUCTURE</p> <p align="center">M 29/150, M 29/151, G 29/29, G 29/30, L 29/143, L 29/153, L 29/154, L 29/137, E 29/1007</p>	Document No.	E-REG-006
		Revision Date	19/06/2023
		Revision No.	1
		Pages (ex. Apps)	54

1 Introduction

Aurene Mining is developing the Mt Ida Gold Project (MIG) (the Project) planned to be a 1.2-1.4 Mtpa gold mining operation using conventional carbon-in-leach technology.

The Project is centred around the Bottle Creek Gold Mine and Mt Ida future project areas in the Eastern Goldfields, 80 km west of Menzies, and 230 km north-northwest of Kalgoorlie with little existing infrastructure. Access to the area is via the sealed Kalgoorlie – Leonora Highway to Menzies, and then along the well-maintained, unsealed Menzies – Sandstone Road to 45 Mile Outcamp, and finally the Mt Ida Road just north of the Copperfield mining centre (**Figure 1**).

1.1 Background

Gold at Bottle Creek was discovered in 1983 and mined by Norgold Ltd between 1988 and 1989 but was prematurely shutdown due to a pit wall failure, mill issues, and a declining gold price in 1990. The project produced 93,000 oz Au from two open pits (VB and Boags) in 18 months of operation. Remaining are two long narrow water filled pits and mullock hills. The mullock has been encased in earth and rehabilitated with relinquishment by Norgold/Rio Tinto in 2001 back to the State of Western Australia.

Aurene Mining’s acquisition of the Project tenements occurred mid-2020 and has since consolidated additional tenements to develop a viable mining operation of mining and processing at the Mt Ida Gold Project.

The MIG Project (Figure 2) comprises the following project areas:

- Bottle Creek consists of Emu, Southwark, Cascade, VB North, VB and Boags
- Mt Ida consists of Tims Find and Shepherds Bush
- Quinns consists of Forest Belle and Boudie Rat.

Stage 1 of the Mt Ida Gold Project Bottle Creek Gold Mine includes mining of Emu, Southwark , VB and Boags pits, processing, and gold smelting with supporting infrastructure for a 24-hour operating workforce with an Accommodation Village and associated infrastructure. Stage 2 will include Mt Ida project area, Tims Find , Shepherds Bush and Quinns deposits.

1.2 Purpose of Document

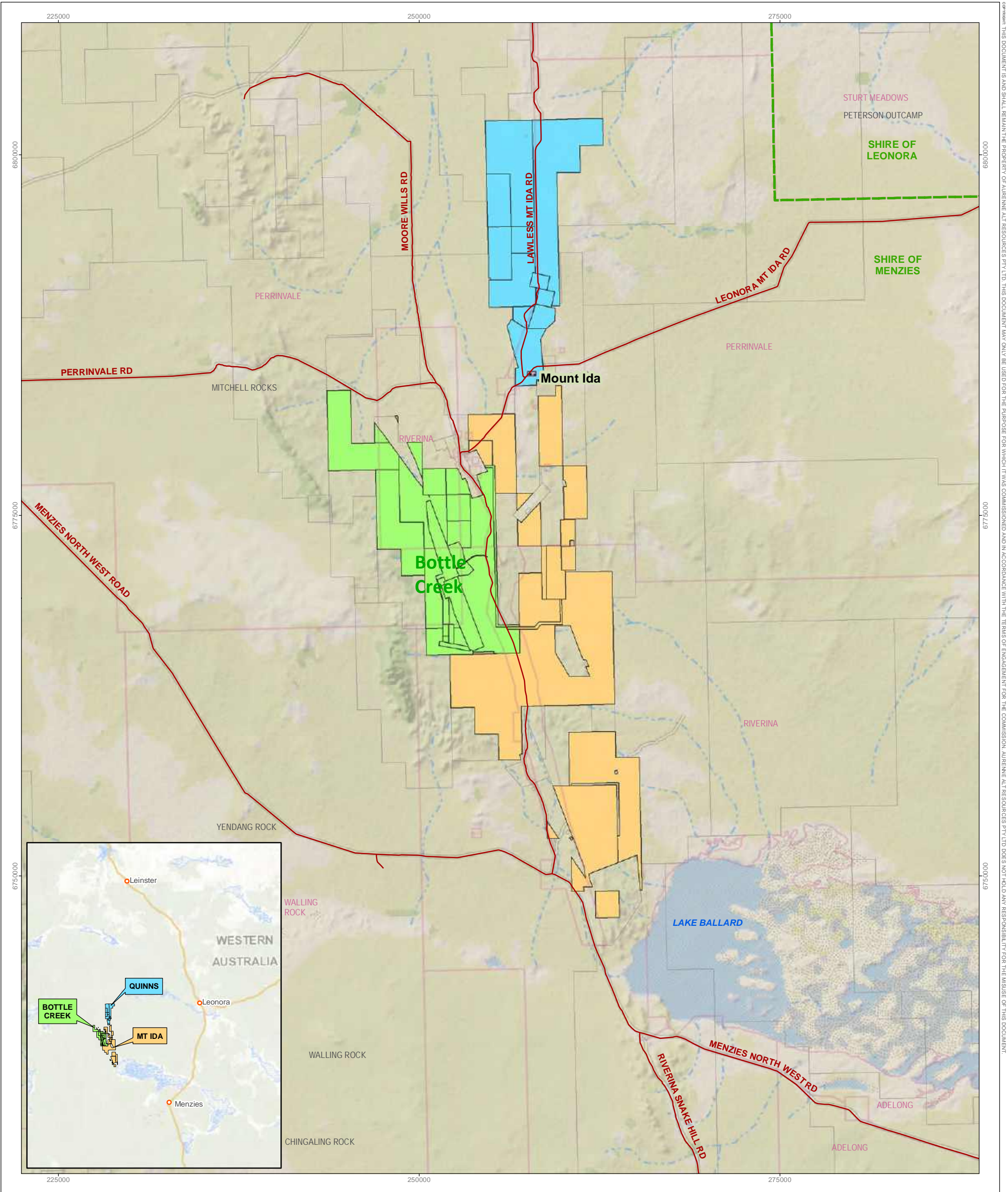
The document details compliance with the requirements of Condition 5 and Condition 10 and 11 Compliance Reporting (non-critical containment infrastructure) of Works Approval 6640/2022/1.

It provides assurance that Aurene is committed to assessing and managing the environmental values and inherent risks of its activities and applies the environmental licensing framework under Part V Division 3 of the Environmental Protection Act 1986 regarding the construction and operation of prescribed premises.

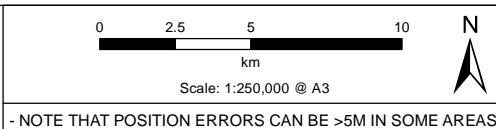
This information is prepared with reference to Department of Water and Environmental Regulation (DWER) Guideline: Industry Regulation Guide to Licensing (June 2019) : Prescribed premises works approvals and licences.

1.2.1 1.2.2 Mining Stage Works Approval

The MIG Project Stage 1 MP/MCP was submitted to DMIRS on 28 November 2021 (EARS application ID 101557). The Stage 1 MP/MCP includes mining, processing, tailings storage, and related services and infrastructure to develop a fully operational gold mine. This Works Approval application is to provide for those activities and infrastructure that meet Schedule 1 thresholds that will require a prescribed premise licence.



- Legend**
- Mt Ida Project Area
 - Bottle Creek Project Area
 - Quinns Project Area
 - Tenement
 - Local Government Authority Boundary
 - Pastoral Station Boundary
 - Road



- NOTE THAT POSITION ERRORS CAN BE >5M IN SOME AREAS



CREATED BY	JOB	DATE	REVISION
ENVIRONMAPS	ST1 MP/MCP	8/09/2021	0

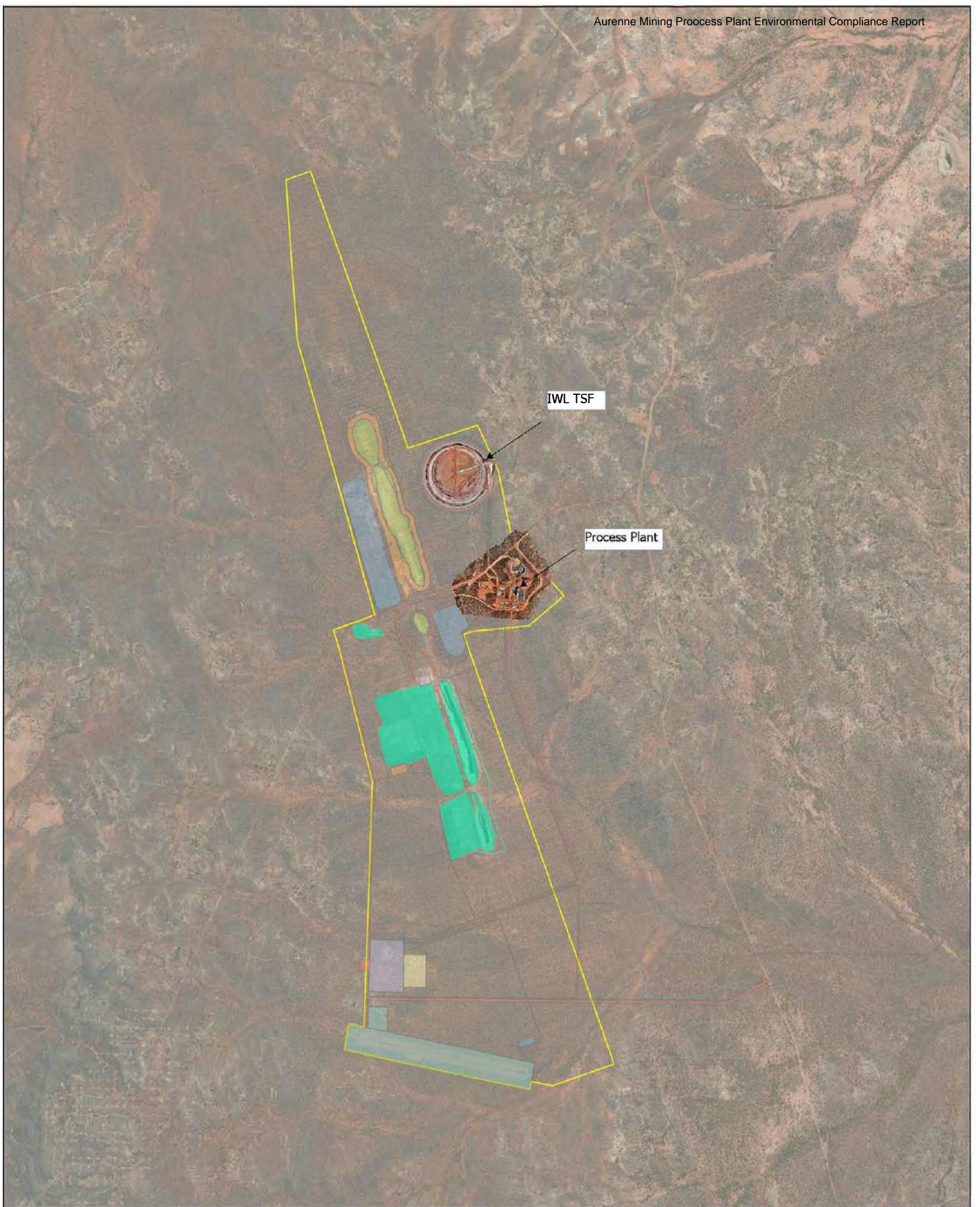
AURENE MINING

FIGURE 1

LOCATION

- PASTORAL STATIONS DPLH 2021
 - TENEMENTS SOURCED DPIRD 2021
 - TOPOGRAPHY SOURCED OPEN SOURCE

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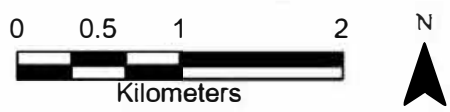


Bottle Creek Gold Mine Indicative Site Layout

- MRF_Cat**
- Airstrip
 - Borefield
 - Building (other than workshop) or Campsite
 - Core Yard

Legend

- Diversion Channel or Drain
- Landfill
- Laydown or Hardstand Area
- Mining Void
- Other Cleared Land
- Plant Site
- Run of Mine Pad
- Sewage Pond
- Tailings or Residue Storage Facility
- Topsoil Stockpile
- Transport or Service Infrastructure Corridor
- Waste Dump or Overburden Stockpile
- Workshop
- Historic (Norgold)
- Prescribed Premise Boundary



Drawn by C Sinclair. Date 6 June 2023.
Scale 1:10,000 A3. Grid GDA 94 MGA Zone 51

Aurene Group Mining
Mt Ida Gold Project

Figure 2 Site Layout

2 Applicant

Aurene Mining is registered to Aurene Group Holdings Pty Ltd. The Aurene Group of Companies hold Aurene Mt Ida Pty Ltd (formerly Aurene Alt Resources Pty Ltd ACN 168 928 416), which holds Aurene MIT Pty Ltd (formerly MGK Resources Pty Ltd ACN 611 002 709). The recent company name changes are reflected in the ASIC extracts (Attachment 1B) and revised Letter of Authorisation is provided in Attachment 1C.

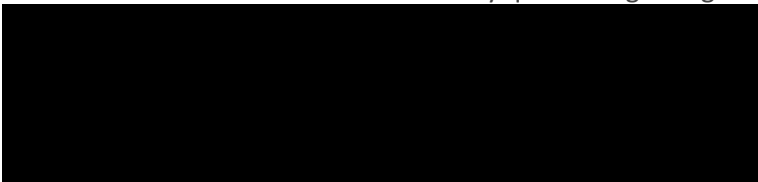
This Works Approval application is made under **Aurene MIT PTY LTD** (formerly MGK Resources Pty Ltd), consistent with other approval instruments for the Project.

Table 1 Proponent hierarchical structure and details

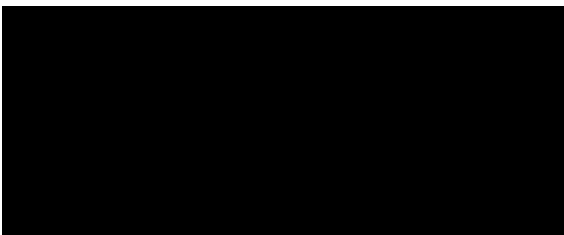
Entity	ACN
Aurene Group Holdings (Aurene Mining)	627 857 176
Aurene Mt Ida PTY LTD	168 928 416
Aurene MIT PTY LTD	611 002 709

Contacts:

Campbell Sinclair is the Environment and Sustainability Manager the Project and compiled this information and is the contact for any queries regarding this submission:



Peter Storey is Chief Operating Officer and the authorised representative for the company and its regulatory application:



3 Tenure

Stage 1 of mining for the Project is centred around the prospects of Bottle Creek; the nominated Prescribed Premise (PP) boundary encompasses the proposed mining, processing, supporting infrastructure, pipelines, and proposed monitoring points.

The PP boundary is provided as spatial files with this application, shown in **Figure 3**; the tenements and activity locations are summarised in **Table 2**.

Table 2 Application area tenements and project activities/locations

Cat #	Tenement	Tenement Start Date	Tenement End Date	MIG reference
5	G 29/30 G 29/29	15/10/2021	14/10/2042	Bottle Creek Processing Plant. Integrated Waste Landform (IWL (tailings storage))
7	G 29/30	15/10/2021	14/10/2042	Bottle Creek Processing Plant (Vat leaching)
64	M 29/150	24/06/1991	23/06/2033	Bottle Creek Waste Facility
85	L 29/145 & L 29/154	17/05/2021	16/05/2042	Bottle Creek Village WWTP & sprayfield

The PP boundary encompasses the boundary of WA W6574-2021-1 (WWTP and irrigation sprayfield). Ultimately all prescribed activities will be included in the one licence for the Project/proposed prescribed premises.

4 Premises

Table 3 summarises the activities and related infrastructure and its proposed location in the Project area relating to this application and proposed Prescribed Premise boundary.

Table 3 Prescribed activities and locations

Cat .	Prescribed premises activities	Location	Document references
5	Processing or beneficiation of metallic or non-metallic ore: premises on which: (a) metallic or non-metallic ore is crushed, ground, milled or otherwise processed; (b) tailings from metallic or non-metallic ore are reprocessed; or (c) tailings or residue from metallic or non-metallic ore are discharged into a containment cell or dam.	G 29/30 G 29/29	10.2.1 Processing Plant Refer to IWL TSF Critical Construction Infrastructure Report
7	Vat or in situ leaching of metal: premises on which metal is extracted from ore with a chemical solution	G 29/30	10.2.2 Vat leaching
64	Class II or III putrescible landfill site: premises on which waste (as determined by reference to the waste type set out in the document entitled "Landfill Waste Classification and Waste Definitions 1996" published by the Chief Executive Officer and as amended from time to time) is accepted for burial	M 29/150 & M 29/151 (future)	10.2.4 Landfill Facility
85	Sewage facility: premises (a) on which sewage is treated (excluding septic tanks);	L 29/145	NA; subject of previous WA application (W6574-2021-1) Attachment 2 Premises Map Attachment 6A Emissions & Discharges
	Sprayfield (b) from which treated sewage is discharged onto land or into waters	L 29/145 & L 29/154	Attachment 7 Siting

5 Prescribed Activities

Table 7 summaries the proposed Project activities that meet thresholds for licensing as a Prescribed Premise.

This section describes the design, construction, operation of the Category 5 Processing and Beneficiation Plant in accordance with Works Approval 6640/ 2022/1

Table 4 Categories and thresholds expected for the Stage 1 Project requirements.

Cat #	Schedule 1 — Prescribed premises Category descriptions	Production or design capacity	MIG estimated throughput	Project location
5	Processing or beneficiation of metallic or non-metallic ore: premises on which: (a) metallic or non-metallic ore is crushed, ground, milled or otherwise processed; (b) tailings from metallic or non-metallic ore are reprocessed; or (c) tailings or residue from metallic or non-metallic ore are discharged into a containment cell or dam.	50 000 t or more pa	Processing: 1.2-1.4 Mtpa SAG Mill with CIP tanks IWL (TSF) designed storage volume 4 Mm ³ . Storage capacity 6 Mt of tailings over a 6-year life assuming an ore processing rate of 1.2 Mtpa, minimum tailings in-situ density of 1.5 t/m ³ (dry) and a beach slope of 1%	Processing Plant/Vat leaching on G 29/30 IWL (TSF) on G 29/29
7	Vat or in situ leaching of metal: premises on which metal is extracted from ore with a chemical solution	5000 t or more pa	Processing: 1.2-1.4 Mtpa	G 29/30
64	Class II or III putrescible landfill site: premises on which waste (as determined by reference to the waste type set out in the document entitled “Landfill Waste Classification and Waste Definitions 1996” published by the Chief Executive Officer and as amended from time to time) is accepted for burial	20 tonnes or more pa (56 m ³)	Expected volume of up to 360 m ³ of waste per year based on 180-person camp generating ~2 m ³ per year	M 29/150 & future on M 29/151 (WRL)
85	Sewage facility: premises (a) on which sewage is treated (excluding septic tanks); or (b) from which treated sewage is discharged onto land or into waters	More than 20 but less than 100 m ³ per day	Combined total is 36-60 m ³ per day. Ranging from early workforce to ultimate capacity WWTP capacity is 70 m ³ per day	L 29/145 (WWTP) & sprayfield on L 29/154

5.1 Bottle Creek Processing Plant (Cat. 5)

The Bottle Creek Processing Plant will be constructed on G 29/29 to the east of the Bottle Creek mining area and is oriented North-South, with the ROM pad and primary crusher pocket established on elevated terrain to the North. It will discharge tailing slurry to an IWL on G 29/30 to the north, and generally consists of:

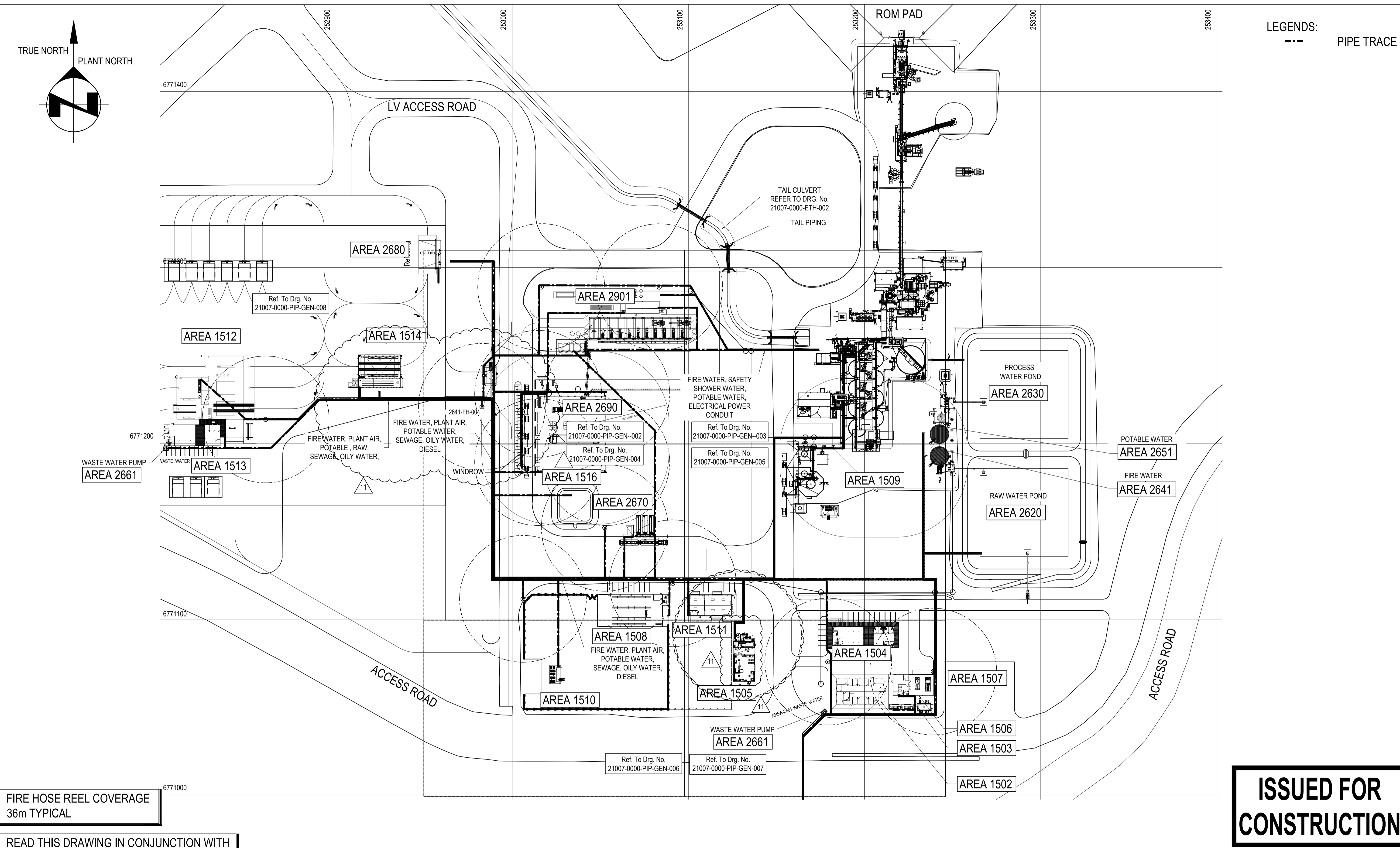
- A Run of Mine (ROM) ore pad accepting delivery of ore by rigid mining trucks of nominal 100 tonne capacity which is stockpiled according to metallurgy and grade and reclaimed by front end loader
- a single stage crushing circuit with a surge bin, which bypasses excess feed to a crushed ore stockpile for front end loader reclaim
- a SAG mill with provision for a future pebble crushing circuit
- mill discharge pumps to a cyclone cluster for classification with underflow able to be split to the SAG mill or to a Ball mill and overflow passing through trash screen
- thickening of leach feed before reporting to a CIP circuit consisting of seven mechanically agitated CIP tanks with intertank screens
- loaded carbon removal from the adsorption circuit by passing slurry over a screen and the carbon acid washed and transferred to an elution column
- a pressure Zadra process elution circuit including a carbon regeneration kiln, electrowinning cells, goldroom and goldroom furnace
- chemical reagent storage (quicklime, sodium cyanide, hydrochloric acid, sodium hydroxide, carbon)
- tailings pumps and piping to the IWL (Refer to Works Approval Application **Section 10.2.3**)

The Bottle Creek Processing Plant is designed for a nominal ore throughput of 1.2 Mtpa configured based on the mineral reserves and resources and the metallurgical test work results. The Processing Plant layout is provided in **Figure 4** and the process flow diagram is provided in **Figure 5**.

The layout provides for the doubling of the throughput capacity with provision for an additional ball mill, thickening capacity and a second CIP train. Additional room is provided for the potential addition of a gold gravity circuit should that be required.

Process reagents and consumables will be required to be prepared and dosed to the plant. Water services will include safety showers and an RO potable system, raw water, process water and fire water.

Monitoring and automated control employed to support the field operators and provide basic management information.

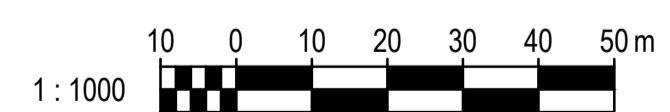


FIRE HOSE REEL COVERAGE
36m TYPICAL

READ THIS DRAWING IN CONJUNCTION WITH
Drg. No. 21007-0000-PIP-GEN-002~008

FIRE, POTABLE, WATER AND SEWAGE LAYOUT

ISSUED FOR CONSTRUCTION



DRAWING No.	REFERENCE DRAWING TITLE	No	BY	DATE	REVISION DETAILS	CHKD	APPR	No	BY	DATE	REVISION DETAILS	CHKD	APPR	PROJ APPR
								7	FRD	31-01-23	LAYOUT UPDATED	RRA	KLB	DRAWN
								6	FRD	27-01-23	LAYOUT UPDATED	RRA	KLB	LRL
								5	FRD	26-01-23	LAYOUT UPDATED	RRA	KLB	26-01-22
								4	AAS	10-10-22	LAYOUT UPDATED	CPD	KLB	CHECKED
								3	PIC	19-09-22	LAYOUT UPDATED	CPD	KLB	ELY
								2	JMC	10-08-22	REVISED LAYOUT	CPD	KLB	KLB
								1	JMC	28-07-22	WASTE PUMP STATION LOCATION UPDATED	ELY	CPD	DESIGNED
								0	JMC	5-06-22	ISSUED FOR CONSTRUCTION	CPD	KLB	DES. APPR

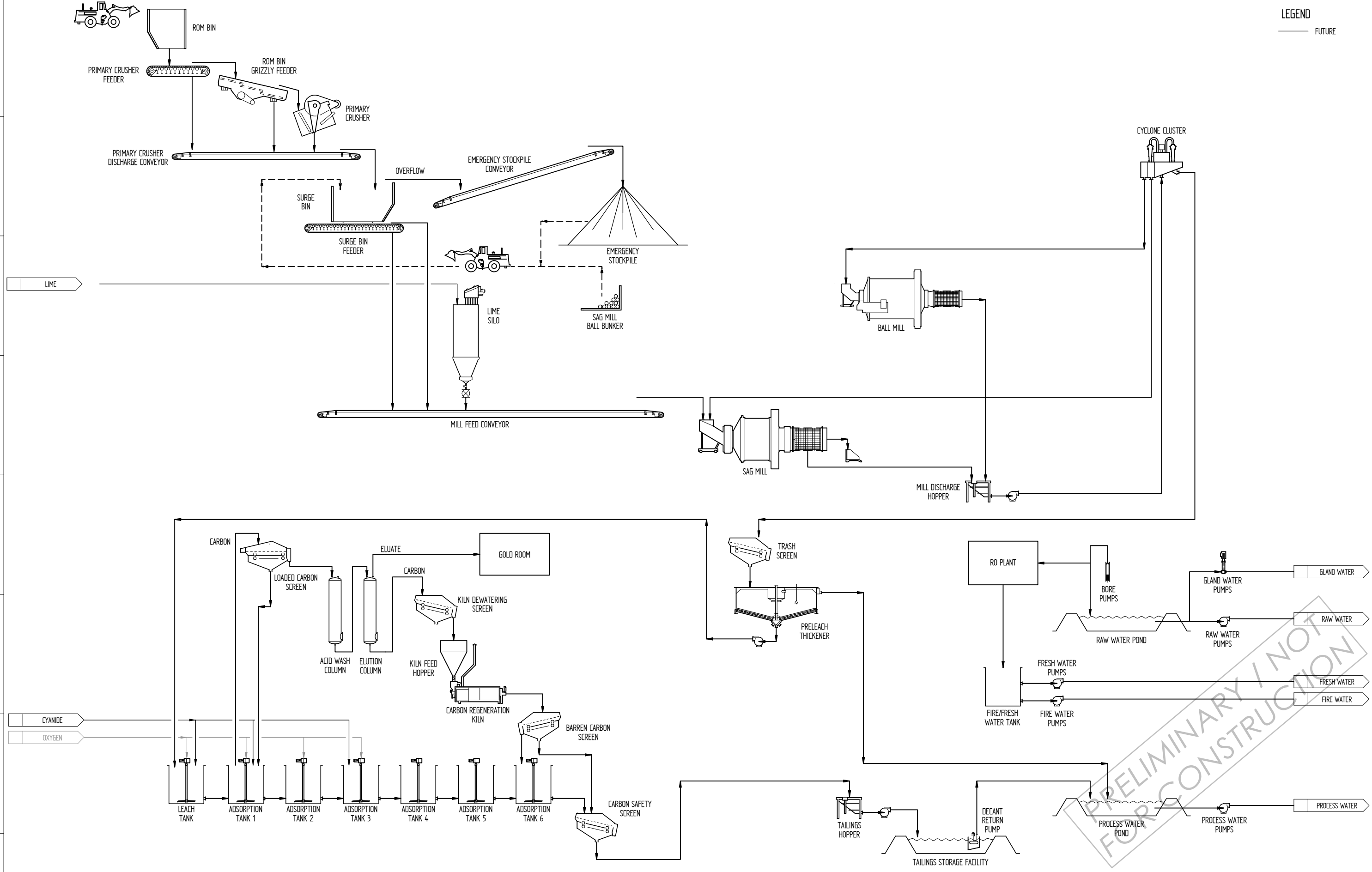


CLIENT **Aurrene Mt. Ida**
 TITLE **MT. IDA GOLD PROJECT UTILITIES AND PROCESS PLANT BURIED SERVICES LAYOUT 1 OF 8**

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 SIZE A1
 ALL DIMENSIONS IN MILLIMETRES
 REV No 0 1 2 3 4 5 6 7 8 9
 DRAWING No 21007-0000-PIP-GEN-001

Figure 5 Plant PFD

LEGEND
 — FUTURE



M112761 - Mt Ida URG1001PFD\BCG 0100\F001.dft - 6/10/2021 - 09:29AM - amehoyne

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AURENE ALT RESOURCES PTY LTD
 MT IDA GOLD PROJECT
 OVERALL PLANT
 PROCESS FLOW DIAGRAM

A1	SCALE	NTS	JOB No	12761	DRG No	BCG 0100-F-001	REV	A
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5.1.1 Single Stage Crushing

Primary size reduction is achieved by single stage jaw crushing. Ore is fed by front end loader on the Run of Mine (ROM) pad to the ROM bin which has an 80-tonne live capacity, with ore drawn from the bin by a 11 kW Metso Outotec apron feeder discharging to a single deck vibrating grizzly. The feeder will be fitted with a variable frequency drive, controlled by the operator to regulate the feed rate to the crusher. The grizzly bars on the feeder have a 75-100mm aperture which removes the undersize from the feed to the crusher, represents approximately 30% of the mass flow with this undersize reporting to the primary crusher discharge conveyor. Grizzly oversize reports to the primary crusher, a 110 kW Weir single toggle jaw crusher with a 750 x 1,050 mm feed opening and Closed Size Setting (CSS) set to deliver a nominal product of P80 150mm. Crusher product reports to the primary crusher discharge conveyor joining the undersize (**Figure 6**)

Dust generation is controlled by dust suppression sprays as necessary. Spillage and run off is captured in a sump area which is pumped to the Grinding Circuit.

Table 5 summarises the Processing Plant design features.

Table 5 Bottle Creek Processing Plant summary

Description	Units	Value
OPERATING SCHEDULE		
Annual throughput rate	tpa	1,200,000
Crushing Circuit	Stages	1
Operating Days per Year	Days	365
Available Operating Hours per Year	Hours	8760
Effective Crusher Utilisation	%	88
Effective Crusher Operating Hours	Hours	7709
Required Crushing Rate	Tph	156
Design Crushing Rate	Tph	180
ROM Top Size	mm	600
Crushing Circuit Product Size P80	mm	150
Rom Bin Live Capacity	m3	50
	Tonnes	80
	Minutes	44.4
PRIMARY FEEDER		
Type		Apron
Width Size	mm	1200
Maximum Capacity	tph	200
VIBRATING GRIZZLY		
Type		Inclined vibrating
Grizzly Bar Spacing	mm	100
PRIMARY CRUSHER		
Type		Single toggle jaw
Nominal Size	mm	762 x 1066
	Inch	30 x 42
CSS	mm	110

5.1.2 Crushed Ore Surge Bin and Reclaim System with Dead Stockpile

Due to the potential stickiness of the ore, a conventional stockpile system with reclaim tunnel has not been adopted, and crushed ore is fed to a surge bin with nominal live capacity of 75 tonne. Ore is drawn from this bin by reclaim feeder to the mill feed conveyor and conditioned with quicklime to raise pH prior to delivery to the SAG mill (**Figure 7**)

Surge bin overflow reports to an Emergency Stockpile Conveyor discharging to the Emergency Stockpile which has a capacity of 1,500 tonnes. When circumstances warrant, this ore is reclaimed from the stockpile by front end loader and placed in the Reclaim feed hopper by way of the access ramp. Mill balls are also loaded at this location. **Table 6** summarises the ore stockpile design.

Table 6 Ore Stockpile Summary

Description	Units	Value
Type		Surge bin with o/f Stockpile
Bin Type		Mass Flow
Angle of Repose	Degrees	37
Draw Down Angle	Degrees	60
Maximum Live Storage Capacity	Tonnes	75
Design Equivalent Milling Capacity	Hours	0.5
Bin Discharge Method		Apron Feeder
Nominal Stockpile Capacity	Tonnes	1500
	Hours	10

5.1.3 Two Stage Grinding and Classification to 45 microns

Secondary size reduction is achieved by means of a wet SAG mill in closed circuit with a wet ball mill. The SAG mill of nominal dimensions 5.2 x 4.2 m and installed motor power of 1800 kW receives crushed ore of nominal P80 150mm at a rate of 150 tonnes per hour with design summary provided in **Table 7**. **Figure 8** details the process flow.

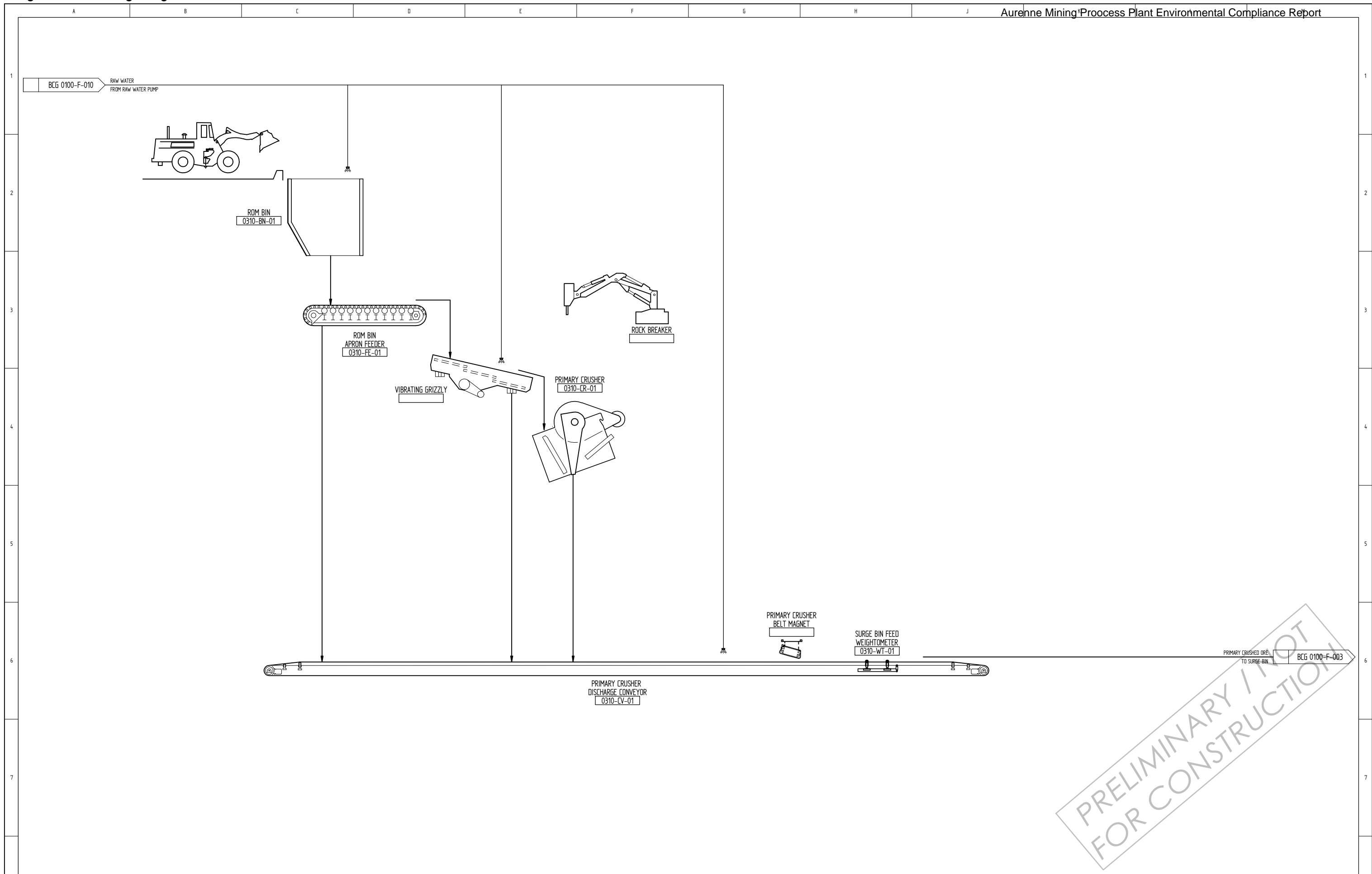
Table 7 SAG Mill summary

Description	Units	Value
GENERAL		
Circuit Type		SAB
Feed Size (F100)	mm	150
Product Size (P80)	um	45
OPERATING SCHEDULE		
Annual Throughput Rate	Tpa	1,200,000
Days per Year	No	365
Availability	%	91.3
Effective Operating Hours per Year	Hours	8,000
Design Treatment rate	Tph	150.0
PRIMARY MILL		
Type		SAG
Nominal Diameter Inside Shell	Metres	5.20
Nominal Effective Grinding length - EGL	Metres	4.20
Nominal Diameter – Inside New Liner	Metres	5.10
Liner Material		Polymet

Description	Units	Value
Mill Speed		Variable
Mill Speed Range	%Cs	60 to 80
Design Mill Speed	%Cs	70
Design Ball Charge	%v/v	18
Maximum Ball Charge	%v/v	20
Design Mill Charge	%v/v	25
Maximum Mill Charge	%v/v	30
Mill Discharge Density	% Solids	70
Total Pinion Power Required	kW	1,200
Consumed Motor Power	kW	1,315
Installed Motor Power	kW	1,800
Discharge Screen Type		Trommel
Trommel Size (dia x length)	Metres	1.8 x 2.17
Trommel Screen Aperture	mm	8
Make Up Ball Size	mm	80
SECONDARY MILL		
Type		Ball Mill
Nominal Diameter Inside Shell	Metres	5.20
Nominal Effective Grinding length - EGL	Metres	7.40
Nominal Diameter – Inside New Liner	Metres	5.10
Liner Material		Rubber
Design Mill Speed	%Cs	75
Design Ball Charge	%v/v	35
Maximum Ball Charge	%v/v	35
Mill Discharge Density	% Solids	70
Total Pinion Power Required	kW	
Consumed Motor Power	kW	
Installed Motor Power	kW	3,500
Discharge Screen Type		Trommel
Trommel Size (dia x length)	Metres	1.8 x 2.17
Trommel Screen Aperture	mm	8
Make Up Ball Size	mm	60
CLASSIFICATION		
Cyclone Size	mm	250
Cluster Size	No.	16
Cyclones Fitted	No.	16
Total Number Operating	No.	12
Total Number Standby	No.	4
Overflow Density	% Solids	25.0
Cyclone Feed Flow	m ³ /hour	503.6
Cyclone Feed Density	% Solids	50.0
Underflow Density	% Solids	70.0
Underflow Solids	Tph	450.0
Underflow Solids	m ³ /hour	412.5
Underflow Water	m ³ /hour	192.9
Underflow Pulp	Tph	642.9
Cyclone Circulating Load	%	300
Operating pressure	kPa	140
Product Size (P80)	um	45

Description	Units	Value
TRASH SCREEN		
Number	No.	1
Type		Horizontal Vibratory
Size (Width x length)	Metres	2.0 x 4.8
Area	m ²	9.6
Screen Feed rate	m ³	503.6
Screen Duty	m ³ /hour/m ²	52.5
Trash Screen Spray Water	m ³	5.0
Screen Deck Type		Poly
Aperture	mm	0.65

Figure 6 Crushing Diagram

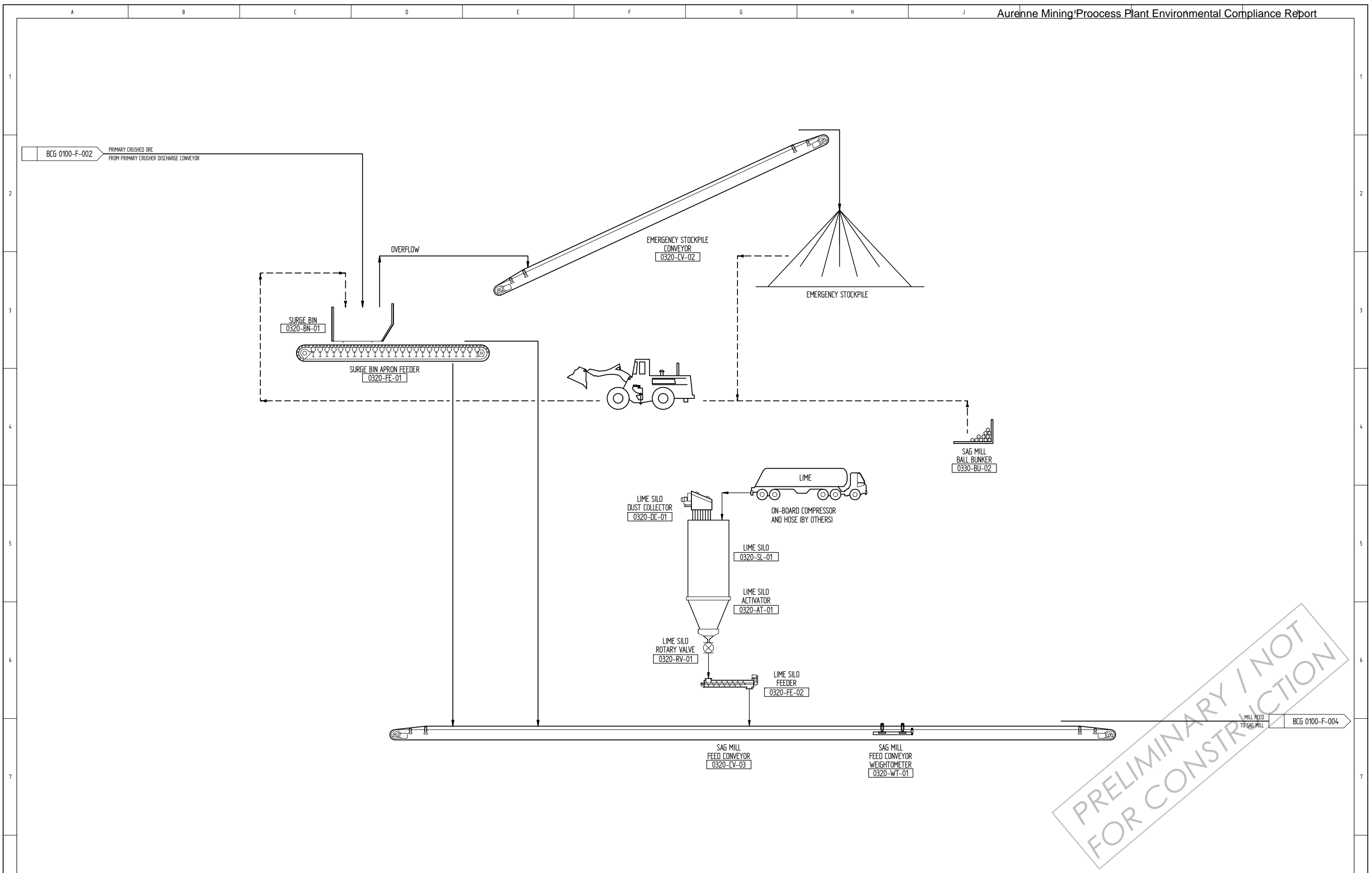


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Figure 7 Ore Handling PFD



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5.2 Vat leaching of metal - Leaching and Adsorption Circuit (Cat 7)

The leaching and adsorption circuit is designed to leach the contained gold and silver metal ions into solution through cyanide dissolution, with the resultant metals adsorbed onto activated carbon for mechanical recovery (**Figure 9 and 10**).

The Mt Ida leach circuit is a hybrid Carbon in Pulp (CIP) circuit comprised of one leach tank and six adsorption tanks of equal size 890 m³ capacity. Residence time is 26 hours.

After being raised to a pulp density of 55% solids in the pre-leach thickener, pulp is transferred to a leach feed box via the thickener underflow pumps where cyanide dosing occurs. The leach feed box also receives goldroom spillage from the gold room sump pump, elution area spillage from the elution area sump pump and barren eluate.

Cyanide dosed pulp is then introduced to the leach tank where precious metals dissolution occurs.

The circuit operates as a counter current flow circuit, with slurry flowing from tank one to tank seven, progressively contacting activated carbon, which is transferred counter currently via intertank screens and pumps from tank seven to tank one. Loaded carbon is recovered from Tank 2, the first adsorption tank, and screened to recover the carbon, which is then transferred to the elution circuit. Regenerated and fresh carbon is pumped into the circuit at Tank 7.

The leached barren slurry from Tank 7 is pumped to the tailings hopper after passing through the carbon safety screen.

The CIP area is a concrete floored and bunded facility with a bund capacity of 110% of the largest CIP tank. The bunded area has design provision for two sumps which are cleared by electric submersible sump pumps, returning material to adsorption tank 2 or 7. All losses from the CIP circuit are therefore contained within the CIP area.

The CIP bunded area, sumps and pumps are subject to routine shift inspection for spillage and sump clearance. Spillage is routinely hosed into sumps to minimise metal losses.

Figures 9 and 10 illustrate the Process Plant Leaching & Adsorption process flow diagram (PFD).

1.1.1 Elution Circuit with Gold and Silver Recovery to Dore

The Elution & Regeneration Circuit PFD is illustrated in **Figure 11**

The recovered carbon is screened with the under flowing slurry returning to CIP Tank 1. The carbon is stored in a hopper until 6 tonnes is collected, when it is discharged into an acid wash column, where a weak 3% HCL acid solution is used to clean the pores of the activated carbon prior to the elution stage. The used acidic solution reports to the tails hopper.

Approximately 900 m³ of Hydrochloric acid is used per elution strip in the Acid Wash.

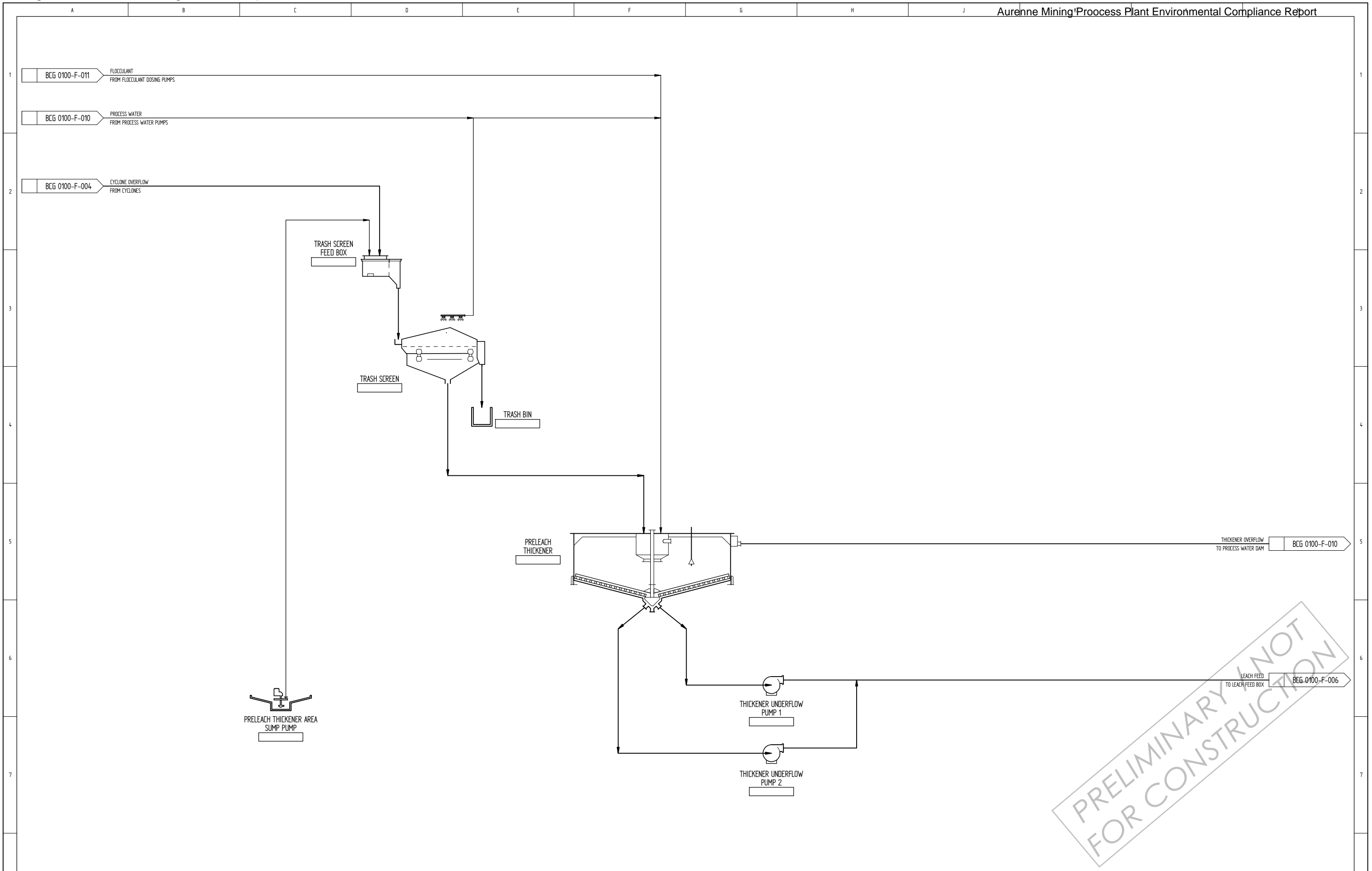
After this, cleaned carbon is transferred to the elution column. In a separate Elution tank, the Eluate is mixed consisting of Fresh Water, Barren Eluate, Sodium Hydroxide (to raise the pH) and Cyanide (to put the gold back into solution).

This mixture is pumped through the through heat exchangers and the elution column, heated by the LNG fired Elution Heater so that the liquid is brought up to a temperature of 90 degrees. Once this temperature is reached, the liquid is also circulated through the electro-winning cells, which plate the

gold on to the cathode plates. This cycle is continued until the eluate solution is devoid of gold from having this plated in the electro-winning cells. The Barren Eluate is pumped to the Eluate tank to be used as makeup. The Carbon is transferred to the Regeneration Kiln Feed Hopper, and slowly brought up to a temperature to drive off any fluid or impurities on the carbon before being discharged into a quenching tank. The regenerated carbon is then sent back to the CIP Circuit via a drainage screen to CIP tank seven.

Sulphonic acid is used occasionally in this circuit to clean the pipes and heat exchangers. This area has a Sump pump which pumps any spillage back to the CIP leach feed distribution box.

Figure 9 Part I Leaching and Adsorption Circuit

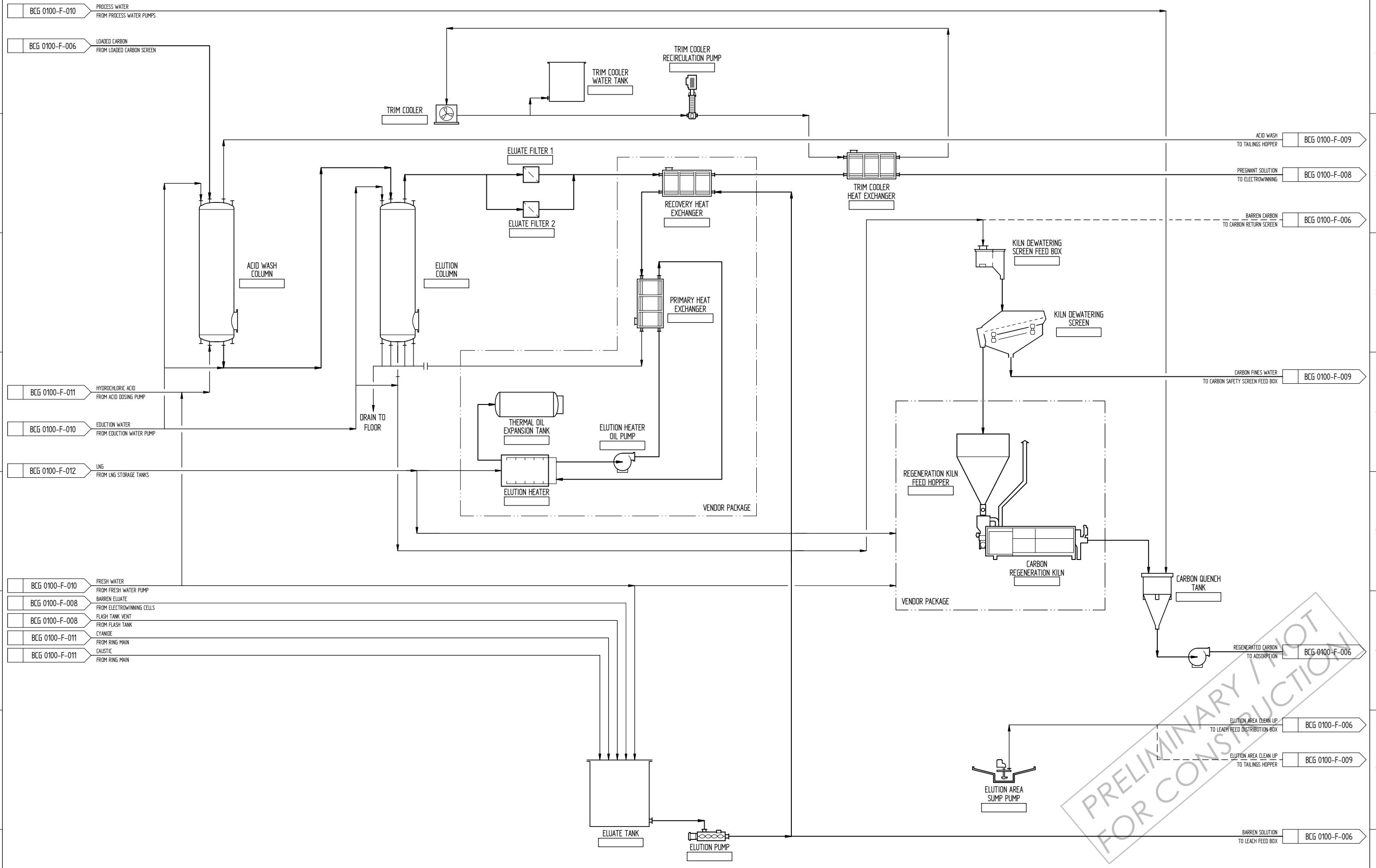


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Figure 11 Elution



- BCG 0100-F-010 FRESH WATER FROM FRESH WATER PUMP
- BCG 0100-F-008 BARREN ELUATE FROM ELECTROWINNING CELLS
- BCG 0100-F-008 FLASH TANK VENT FROM FLASH TANK
- BCG 0100-F-011 CYANIDE FROM RING MAIN
- BCG 0100-F-011 CAUSTIC FROM RING MAIN

REGENERATED CARBON TO ADSORPTION BCG 0100-F-006

ELUTION AREA CLEAN UP TO LEACH FEED DISTRIBUTION BOX BCG 0100-F-006

ELUTION AREA CLEAN UP TO TAILINGS HOPPER BCG 0100-F-009

BARREN SOLUTION TO LEACH FEED BOX BCG 0100-F-006

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AURENNE ALT RESOURCES PTY LTD
 MT IDA GOLD PROJECT
 ELUTION AND REGENERATION
 PROCESS FLOW DIAGRAM

A1 SCALE NTS JOB No 12761 ORG No BCG 0100-F-007 REV A

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1.1.2 Electrowinning and Goldroom

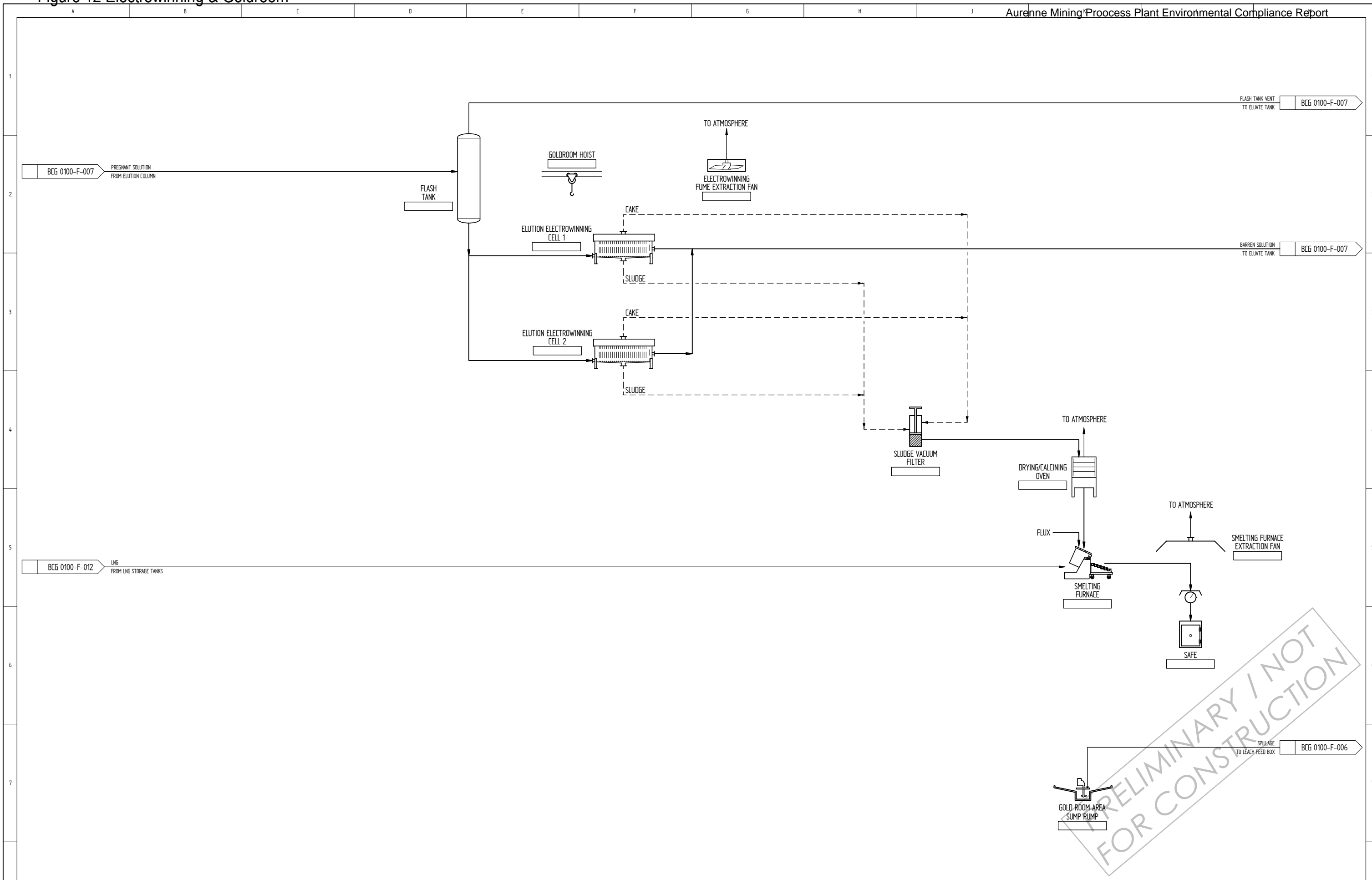
The Electrowinning and Intensive Cyanidation PFD is provided in **Figure 12**.

Material plated onto the cathodes on the electro-winning cells is cleaned off the cathode plates and flows to a settling cone. The material from the settling cone is removed from the bottom of the cone and dried in a drying oven to remove moisture.

The dried material is then placed in the furnace with measured amounts of Flux materials – Silica, Soda Ash, Borax, and Sodium Nitrate. The furnace is then heated to approximately 1200 degrees. As the gold and silver bearing material melts, the fluxes aid the separation of the heavier gold from the other material by improving the viscosity of the melt and assisting in purifying this. Once the molten separation has had time to occur, the furnace is tilted into the ingot moulds, which are filled by the Slag material on the top of the furnace, and the gold at the bottom. The Slag material, once cooled, is returned to the grinding mill so any remnant gold can be recovered.

This area has a sump pump which returns any spillage or wash down to the CIP leach feed distribution Box, after passing through a gold trap for security reasons.

Figure 12 Electrowinning & Goldroom



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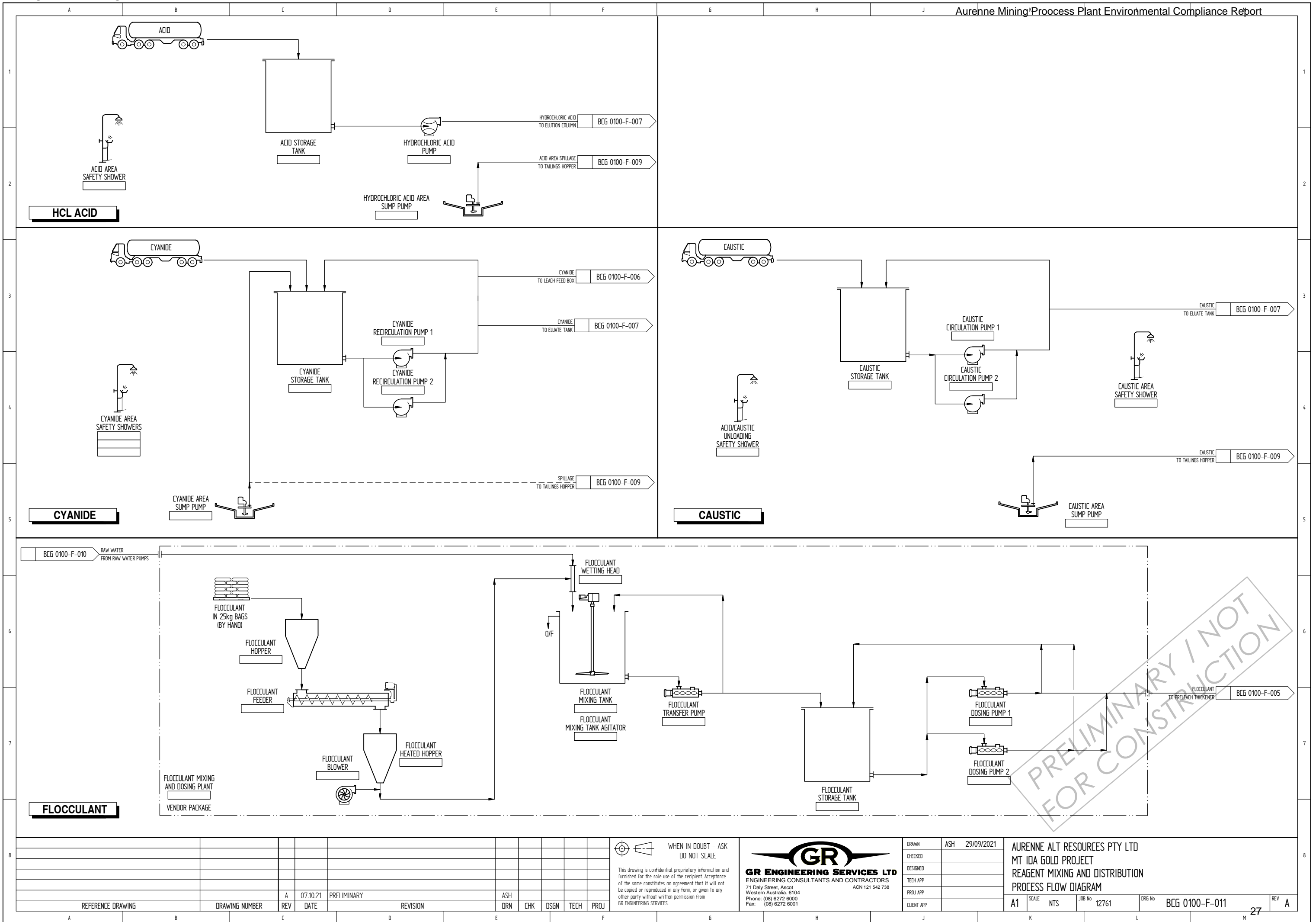
1.1.3 Reagent Use and Management

Reagent mixing and distribution PFD is shown in **Figure 13** and used in the processing plant

- are:
- **Quicklime** (80% calcium oxide) is used to modify ore pH and is stored in a 100 tonne steel silo adjacent to the mill feed conveyor. The quicklime is delivered by road tanker and loaded pneumatically to the silo every 5 days approximately. The quicklime silo has a filter on top (baghouse) to relieve air introduced into the silo during filling and ensure no quicklime escapes to the atmosphere. The system bottom feeds the CaO to the ore on the mill feed conveyor via a mixing arrangement. There is no specific containment under the quicklime silo.
 - **Cyanide** (Sodium cyanide) will be delivered by truck in liquid form as 29% CN by 16m³ isotainer and transferred to a 140m³ holding tank. Cyanide solution is pumped as required to the leach circuit using a variable speed pump via stainless steel piping specifically designed for cyanide distribution and containment. The cyanide storage tank of 140m³ capacity and the caustic soda tank of 30 m³ capacity are contained in a common concrete bund of 168 m³ capacity designed to contain the largest tank (cyanide) to conform to the ICMC 120% requirement. The horizontal extent of the bund from the tank wall position is designed by applying the tan theta rule to potential side wall tank discharge. The bunds are constructed with collection sumps and recovery pumps which discharge sump solutions to the CIP circuit.
 - **Caustic soda** (sodium hydroxide) Liquid Caustic as 50% NaOH will be delivered by truck in 16m³ isotainers and transferred to a 30m³ storage tank located in the common cyanide – caustic banded reagents area. The caustic tank is dual walled and will deliver caustic to the elution circuit via positive displacement pumps. The bunding arrangements and solution recoveries are described in the previous section.
 - **Hydrochloric acid** (HCL) as 28% HCL will be delivered to site truck in 16 m³ isotainer and transferred to a 30m³ tank dual walled tank and bund situated in a separate area from caustic and cyanide storage. The HCL bund volume is designed as 110% containment or 33 m³ and the tan theta rule will apply to bunding extents from the tank wall positions. The hydrochloric acid will be delivered to the circuit via metering pump and (PVC) pipelines conforming to engineering standards.
 - **Activated carbon** is delivered to site in plastic lined bulka boxes and stored undercover in the site warehouse until required.
 - **Grinding media** is delivered to site in media bulka bags or in 44 gallon drums (205 L). These are stored in the site warehouse or maintenance yard.
 - **Flocculant** delivered as a dry powder in 1 tonne packages of 40 x 25kg bags. Bags are emptied to the flocculant mixing system which prepares a flocculant solution for use in the Pre-Leach Thickener. The flocculant mixing system is located inside the contiguous CIP – thickener bunding. This area has a dedicated sump and electric vertical spindle sump recovery pump which discharges to the thickener or the CIP circuit.

Chemicals (and hydrocarbon, fuels) transport, storage and use will be according to, and regulated under Dangerous Goods Licence (in application with external DG SME consultant).

Figure 13 Reagent Use PFD



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A1	SCALE	NTS	JOB No	12761	DRG No	BCG 0100-F-011	REV
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5.3 Water Services

Two streams of water are required for the Project: process water, and potable water. The source of this water will be ultimately determined by the availability of water, the distance to the mine, the quality of the water and cost of treatment.

5.3.1 Process Water

Figure 14 depicts water PFD for the plant. There will be two ponds that manage the Process Plant water requirements: the Raw Water Pond and the Process Water Pond. Both will be fenced, monitored for overflow, inspected daily, and lined with High Density Polyethylene (HDPE) (min. 2 mm). An operational freeboard of 500 mm will be always maintained.

At Stage 1, consistent with the submitted Mining Proposal and Mine Closure Plan (MP/MCP), raw water will be obtained from dewatering from existing pit lakes (VB & Boags open pits) via diesel-powered pumps and HDPE pipes to refill the raw water pond.

Future, potential dewatering from VB North and Emu pits will provide raw water once groundwater is intercepted during mining. Water from in-pits will be pumped and piped to the Processing Plant as per general arrangement **Figure 14**. Should dewatering volumes be larger than the process water requirement, surplus water can be managed by in-pit storage accommodated in the existing VB and Boags pits that have a significant freeboard capacity and given the high evaporation rates of the region, and are not at risk of overtopping given the low volumes within, the low flow volumes expected from VB North and Emu, and the significant dewatering proposed to meet the process water demands of the Plant.

In addition, as water in the existing pits is being diminished, exploration for a suitable borefield will be the subject of a Programme of Works approval (DMIRS) and will require a licenced amendment to existing RIWI Act GW license.

The Process Water Pond will also accept decant return water from the IWL once suitably constructed and commissioned and with an expected return time of 30 days.

5.3.2 Process Water Pond

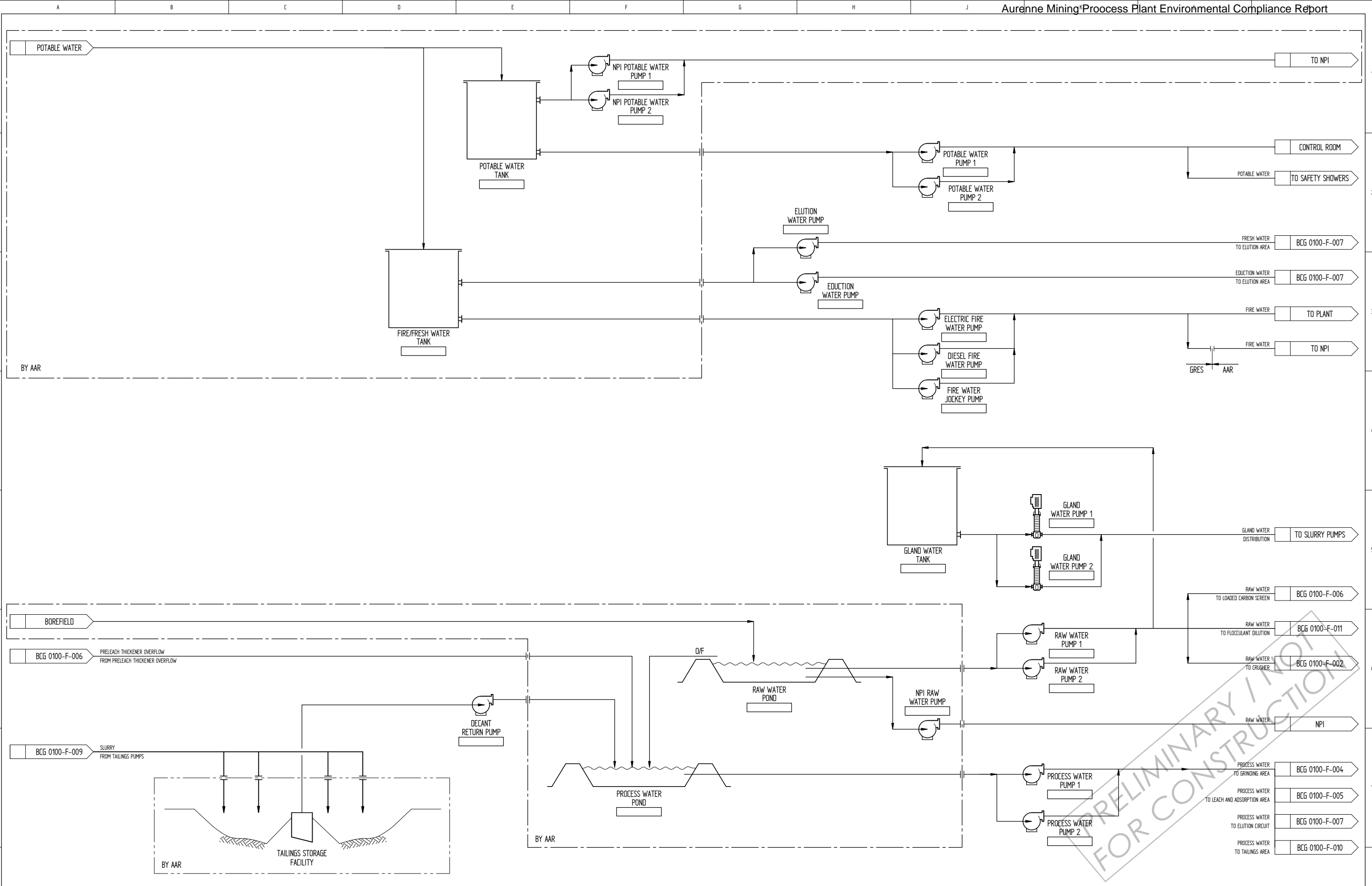
The Process Water Pond is designed to hold 5,000 m³ of process water and is constructed from engineered compacted earthen walls and lined with 2 mm HDPE. The process water pond receives pumped decant return water from the IWL, overflow from the raw water pond and valved gravity fed supernatant water from the pre leach thickener overflow. The Process Water Pond is designed and will be constructed with an engineered, lined overflow structure to an integrated and lined emergency sump.

However, should there be an uncontrolled event such that the process water pond is receiving excess water than can be distributed to the process plant, set point controls to manage the designated freeboard below the emergency discharge will divert pumped process water discharge to the IWL through a separate dedicated (interconnected and valved) return line to maintain the desired freeboard. Should one pump fail, the second, standby pump will be used.

5.3.3 Raw Water Pond

The Raw Water Pond is designed to hold 5,000 m³ of raw water and is constructed from 2 mm thick HDPE. The pond will accept mine dewater (Boags & VB initially; VB North & Emu after 6-12 months) and bore water (as borefield is developed in 3-6 months). Inflow to the raw water pond is therefore completely controlled using pumps from either mine dewatering or the borefield. Controlled overflow of raw water to supplement the process water pond is achieved via a 2 mm thick HDPE lined spillway and through the management of the borefield or mine dewatering pumps. There is no other designed overflow structure, with all overflow reporting to the Process Water Pond. The raw pond overflow contingency is therefore managed by the provisions of the process water pond overflow contingencies.

Figure 14 Water Storage and Reticulation PFD



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6 Non-critical Infrastructure audit

Condition 10 of Works Approval 6640/2022/1 requires an audit of the of the design and construction/installation requirements as shown in **Table 8**. **Table 9** provides the Audit Summary Table and Section 7 summarises the installed infrastructure with photos and drawings.

Table 8 : Design and construction/installation requirements

	Infrastructure	Design and construction requirements	Infrastructure location
1	Gold processing plant and associated infrastructure	(a) Gold processing plant comprises the following infrastructure and equipment: <ol style="list-style-type: none"> i. Run of mine (ROM) pad; ii. Crushing circuit – primary jaw crusher and secondary cone crusher; iii. SAG mill; iv. Carbon in pulp (CIP) circuit; and v. Elution and gold recovery circuit. (b) Plant area to be constructed upon a concrete pad (c) Reagents, dangerous goods, and diesel to be stored in concrete bunded areas; (d) Carbon in Pulp (CIP) circuit to be located on a concrete floor and bunded with a capacity of 110% of the largest CIP tank; (e) Surface water diversions/sumps to be installed to divert stormwater away from operational areas; and (f) Layout of the processing plant to be in accordance with Figure 7 in Schedule 1.	As shown in Figure 1 and Figure 7 of Schedule 1
2	Process water pond	(a) HDPE lined (2.0 mm minimum) with a low permeability liner of 1×10^{-9} m/s and designed to contain a one in one hundred-year 72 hours ARI rainfall event; (b) Constructed to maintain a minimum 300 mm freeboard; and (c) Layout in accordance with Figure 7 of Schedule 1.	
3	Raw water pond	(a) HDPE lined (2.0 mm minimum) with a low permeability liner of 1×10^{-9} m/s; (b) Constructed to maintain a minimum 300 mm freeboard; and (c) Layout in accordance with Figure 7 of Schedule 1.	

Table 9 Design and Construction Audit

Infrastructure	Design and construction requirements	Status	Evidence	Comments
1. Gold processing plant and associated infrastructure	a) Gold processing plant comprises the following infrastructure and equipment: I. Run of mine (ROM) pad; II. Crushing circuit – primary jaw crusher and secondary cone crusher; III. SAG mill; IV. Carbon in pulp (CIP) circuit; and V. Elution and gold recovery circuit.	Compliant	PIE Report No 0104 -RP-011 Aerial Photo Figure 15 with as built designs PIE certified construction drawing 21007-0000-GEN-002 Figure 16 PIE Certified Plant layouts Figure 17, 18, 19	ROM pad will be constructed in stages to the requirements of the mining schedule.
	b) Plant area to be constructed upon a concrete pad	Compliant	Mill, Tailings thickener, CIP circuit are all on concrete pads and bunded – Photos 1, 7, 8 and 9 PIE Report No 0104 -RP-011 Section 3.2 , 3.3, 3.5 , 3.5	
	c) Reagents, dangerous goods, and diesel to be stored in concrete bunded areas	Compliant	Photos of bunded ancillary services (Photos 2, 3, 4, 5) PIE Report No 0104 -RP-011 Section 3.6	
	d) Carbon in Pulp (CIP) circuit to be located on a concrete floor and bunded with a capacity of 110% of the largest CIP tank	Compliant	CIP circuit is located on a concrete pad and bound. PIE Report No 0104 -RP-011 Section 3.4	
	e) Surface water diversions/sumps to be installed to divert stormwater away from operational areas	Not completed	N/A	Diversion drains have not been completed to date due to the availability of equipment. Diversion drains will be completed during time limited commissioning and before the summer wet season (December to March). A separate compliance document will be submitted during TLO to address this requirement.
	f) Layout of the processing plant to be in accordance with Figure 7 in Schedule 1.	Compliant	PIE Report No 0104 -RP-011 – compliance with design – Section 5.1 Aerial Photo Figure 15 with as built designs PIE certified construction drawing 21007-0000-GEN-002 Figure 16 PIE Certified Plant layouts Figure 17, 18, 19	Non-processing infrastructure HV/LV workshop was moved to avoid a P1 plant <i>Jacksonia ianacarpa</i> which was present in large clusters. The process plant layout remains compliant.
2. Process water pond	a) HDPE lined (2.0 mm minimum) with a low permeability liner of 1 x 10 ⁻⁹ m/s and designed to contain a one in one hundred-year 72 hours ARI rainfall event;	Compliant	Certification by PIE. PIE Report No 0104 -RP-011 Section 3.7 PIE Certified layouts Figure 21	
	b) Constructed to maintain a minimum 300 mm freeboard;	Compliant	Certification by PIE. PIE Report No 0104 -RP-011 Section 3.7	
	c) Layout in accordance with Figure 7 of Schedule 1.	Compliant	PIE certified construction drawing 21007-0000-GEN-002 Figure 16 PIE Certified Plant layouts Figure 21 PIE Report No 0104 -RP-011 Section 3.7	
3. Raw water pond	a) HDPE lined (2.0 mm minimum) with a low permeability liner of 1 x 10 ⁻⁹ m/s;	Compliant	Certification by PIE. PIE Report No 0104 -RP-011 Section 3.8 PIE Certified Plant layouts Figure 21	
	b) Constructed to maintain a minimum 300 mm freeboard	Compliant	Certification by PIE. PIE Report No 0104 -RP-011 Section 3.8 PIE Certified Plant layouts Figure 21	
	c) Layout in accordance with Figure 7 of Schedule 1.	Compliant	PIE certified construction drawing 21007-0000-GEN-002 Figure 16 PIE Report No 0104 -RP-011 Section 3.8 PIE Certified Plant layouts Figure 21	

7 Summary of design and construction requirements

7.1 Gold processing plant and associated infrastructure

The processing plant has been constructed as per Figure 7 in Schedule 1 Works Approval 6640/2022/1 with the following components:

- Run of mine (ROM) pad;
- Crushing circuit – primary jaw crusher and secondary cone crusher;
- SAG mill;
- Carbon in pulp (CIP) circuit; and
- Elution and gold recovery circuit.

The design and construction has been designed and certified by PIE Engineering

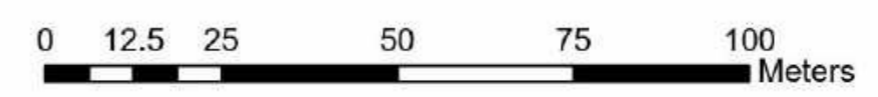
Figure 15 shows an aerial top-down shot of the plant in its approved configuration. The final approved for construction layout is in **Figure 16**.

Refer also to PIE certified plant layouts **Figure 17, 18, 19**



Legend

— Project Survey As Built

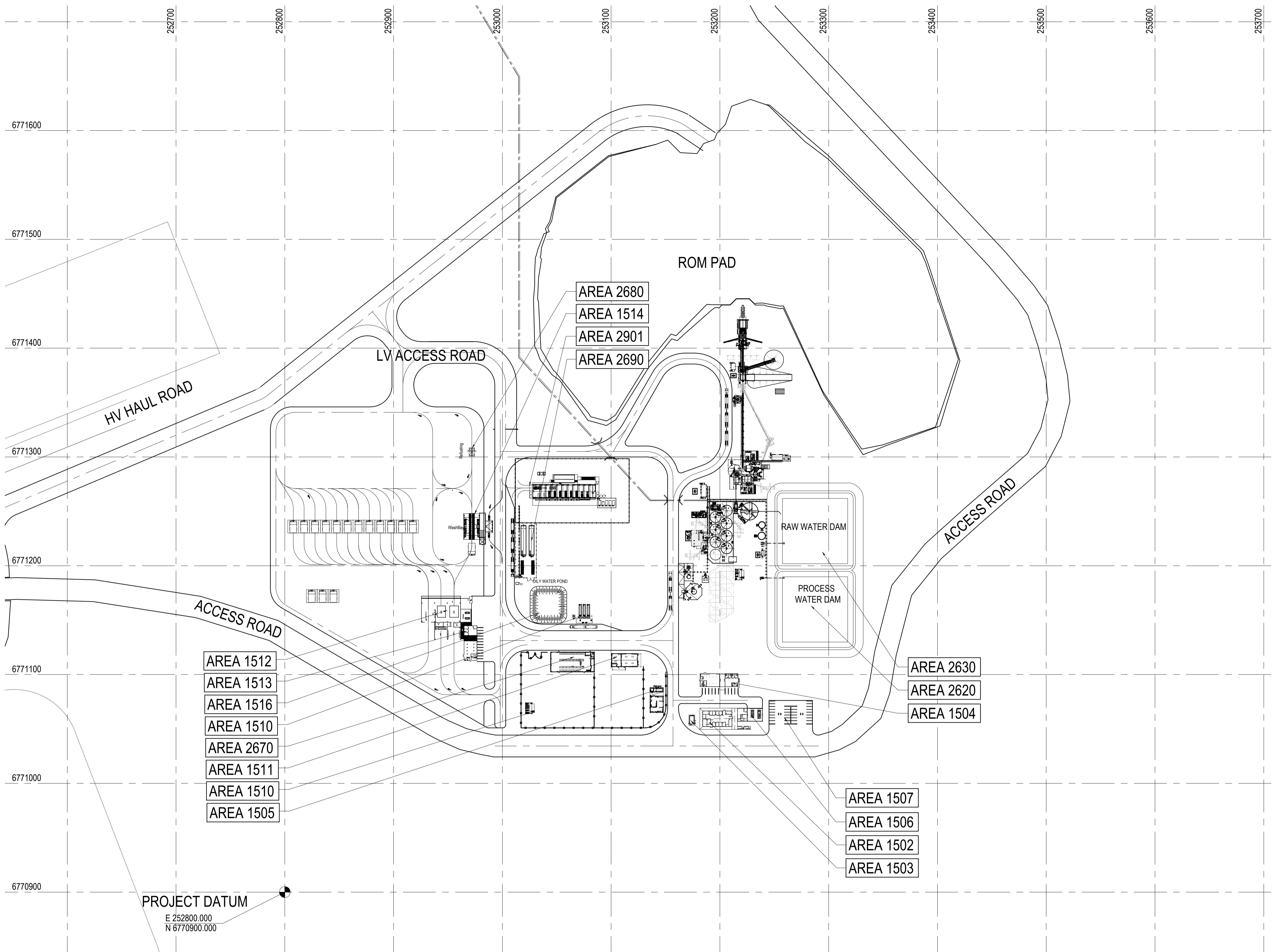
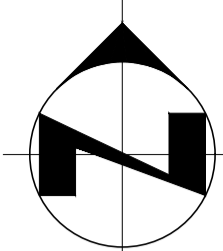


Aurene Group Mining
Mt Ida Gold Project
Bottle Creek Mine

Drawn by C Sinclair. Date 10 July 2023.
Scale 1:1000 A3. Grid GDA 94 MGA Zone 51

Figure 15 Plant Aerial





PLANT INFRASTRUCTURE LAYOUT

PROJECT CONTROL POINT, SP-001
 SITE COORDINATES LOCAL PROJECT CONTROL POINT
 Coordinate System: - WGS-84 /UTM COORDINATES
 E 252800.000 N 6770900.000 E 000.000, N 000.000
 EL +476.000 NOM (To Be Verified) RL 0.000 NOM (To Be Verified)
 LOCAL PLANT GRID ROTATED 20.00° NORTH
 REFER DRG. 21007-0000-ETH-001

ISSUED FOR REVIEW
 NOT FOR CONSTRUCTION

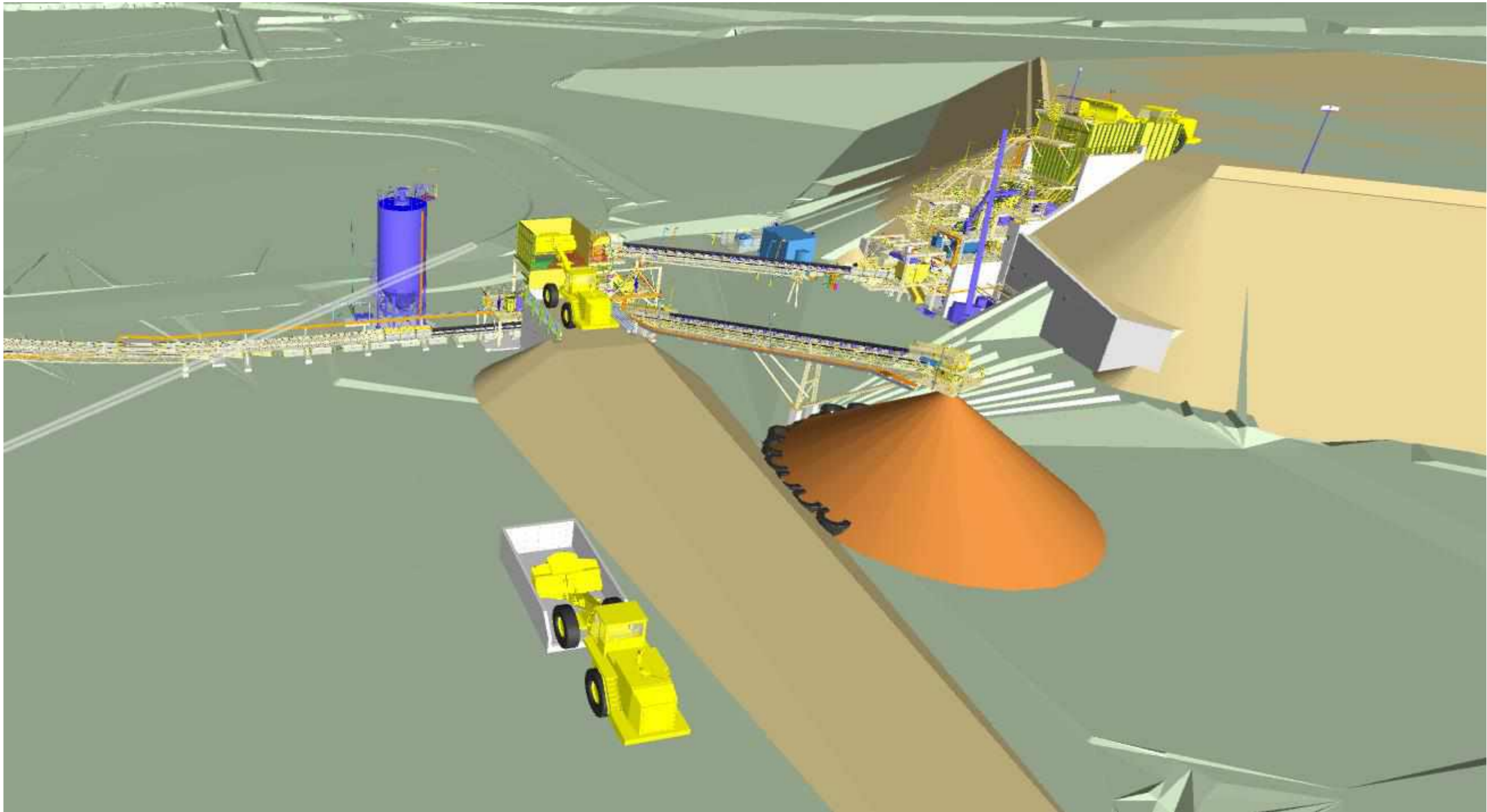


DRAWING No.	REFERENCE DRAWING TITLE	No	BY	DATE	REVISION DETAILS	CHKD	APPR	No	BY	DATE	REVISION DETAILS	CHKD	APPR	PROJ APPR
21007-0000-GEN-001	OVERALL SITE LAYOUT													



CLIENT	Aurene Mt. Ida	SCALE	1:1500	SIZE	A1									
TITLE	MT. IDA GOLD PROJECT PLANT INFRASTRUCTURE LAYOUT OVERALL GENERAL ARRANGEMENT	ALL DIMENSIONS IN MILLIMETRES												
		REV No	J	K	L	M	N	P	Q	R				
		DRAWING No	21007-0000-GEN-002											





7.1.1 Sag and Ball Mills

Works in the SAG and Ball Mill area consist of the following:

- a) The SAG and Ball Mills are situated on engineer designed concrete pads and plinths.
- b) Safety features to prevent personnel injury around the SAG and Ball mills include handrails, guards and suitable safety signs.
- c) Electrical wiring and installations are protected from the environment. All electrical boxes are weatherproof and correctly identified with safety signs warning of any electrical danger.



Photo 1 SAG and Ball Mills on bunded concrete pad

7.1.2 Bunded Chemical Storage Areas

Works in the Reagents area consist of the following:

- a) The reagents stored on site are Quicklime (CaO), Sodium Hydroxide (NaOH), Cyanide (CN⁻), Hydrochloric Acid (HCl), Nitric Acid (HNO₃), Hypochlorite Solution (ClO⁻), Carbon (C), compressed Oxygen (O₂) and Flocculant. NaOH, HCl and CN⁻ reagents are stored in the plant reagents area and consist of three (3) separately bunded tanks. Quicklime is stored in a silo for direct feed onto the mill feed conveyor (Photo 2 and 3).
- b) The Reagent Store has storage allocated for NaOH, HCl and HNO₃ in plastic totes for use in the laboratory, fresh Carbon in bulk bags and Flocculant in smaller bags. The acids and NaOH are stored in bunds separated by a 5 meter space where the Carbon and Flocculant are stored in the middle bund of the Reagent Store. The Reagent Store outer bund wall is 400mm high (Photo 6).Figure
- c) HNO₃ and NaOH is used and stored in the Laboratory. Larger quantities of these reagents are stored outside on spill containment bunded pallets. The outside storage areas of HNO₃ and

NaOH are more than 5 meters apart. Smaller quantities of laboratory reagents are stored inside in a DG cabinet.

- d) For safety reasons a 5 meter separation distance has been maintained between the Sodium Cyanide (NaCN) and Hydrochloric Acid (HCl) solutions. The NaOH, HCl and CN- reagent storage tanks are contained within concrete bunds sized to contain 110% of the largest tank volume including from wall spray.
- e) Safety features to prevent personnel injury around the Reagents storage area include suitable safety signs to warn of the danger from reagents and safety showers.
- f) Bulk diesel is stored in self-bunded storage tanks. The unloading slab in front of the bulk storage is graded to drain to the waste oil sump. The heavy vehicle fuelling slab is drained to the heavy vehicle washdown facility which has an oily water separator. The power station day tank and waste oil tank are contained within concrete bunds (Photo 4 and 5)



Photo 2 Hydrochloric acid tank bunding



Photo 3 Caustic alkali tank bunding



Photo 4 Diesel Storage

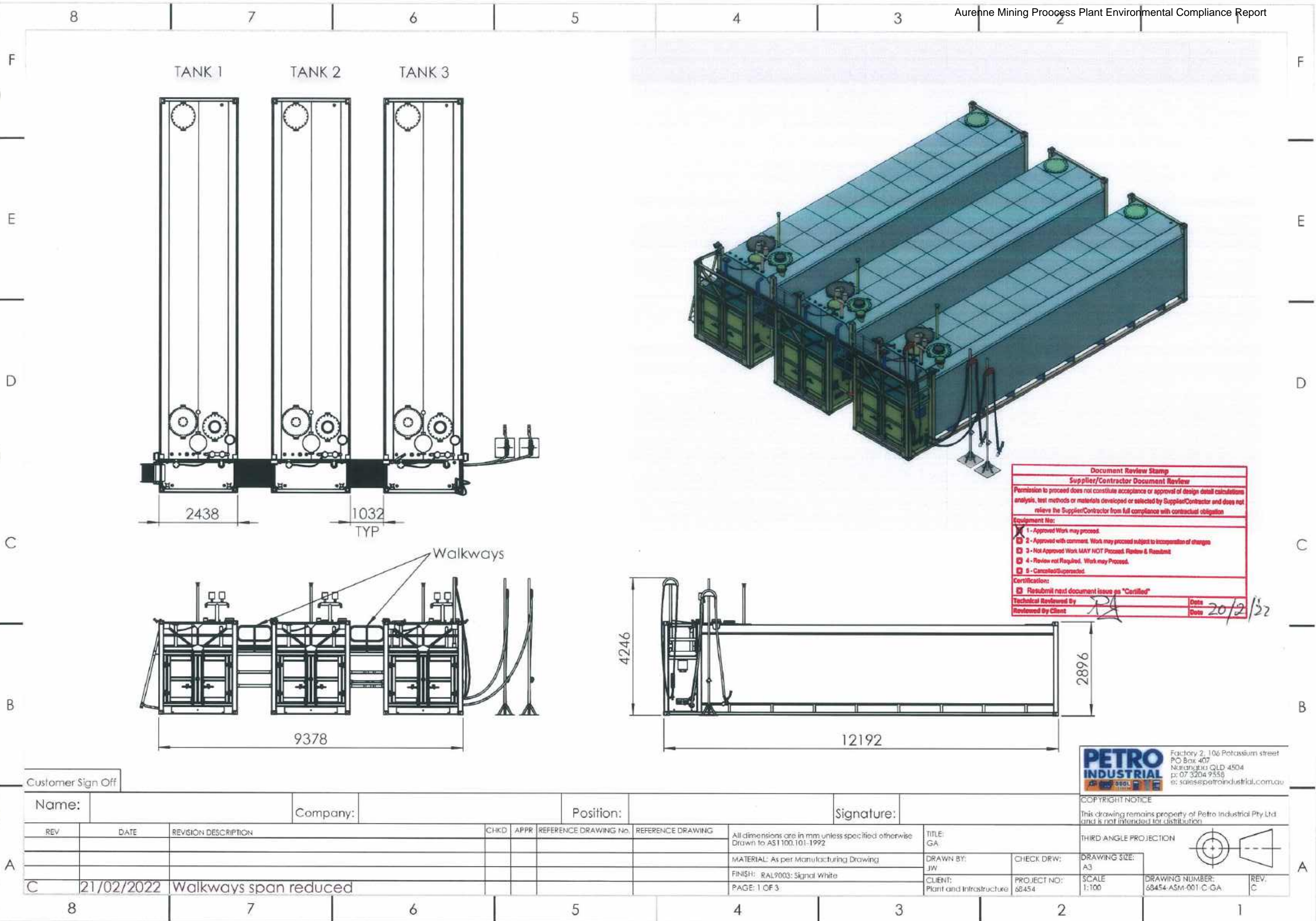


Photo 5 Spillage sump



Photo 6 Reagents shed with bunding

Figure 19 Diesel Isometric and Layout



Document Review Stamp
Supplier/Contractor Document Review
 Permission to proceed does not constitute acceptance or approval of design detail calculations analysis, test methods or materials developed or selected by Supplier/Contractor and does not relieve the Supplier/Contractor from full compliance with contractual obligation

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							All dimensions are in mm unless specified otherwise Drawn to AS1100.101-1992	JW		A3	1:100	68454-ASM-001-C-GA	C
C	21/02/2022	Walkways span reduced					MATERIAL: As per Manufacturing Drawing FINISH: RAL9003: Signal White PAGE: 1 OF 3	Plant and Infrastructure	PROJECT NO: 68454				

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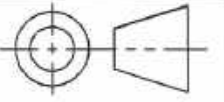
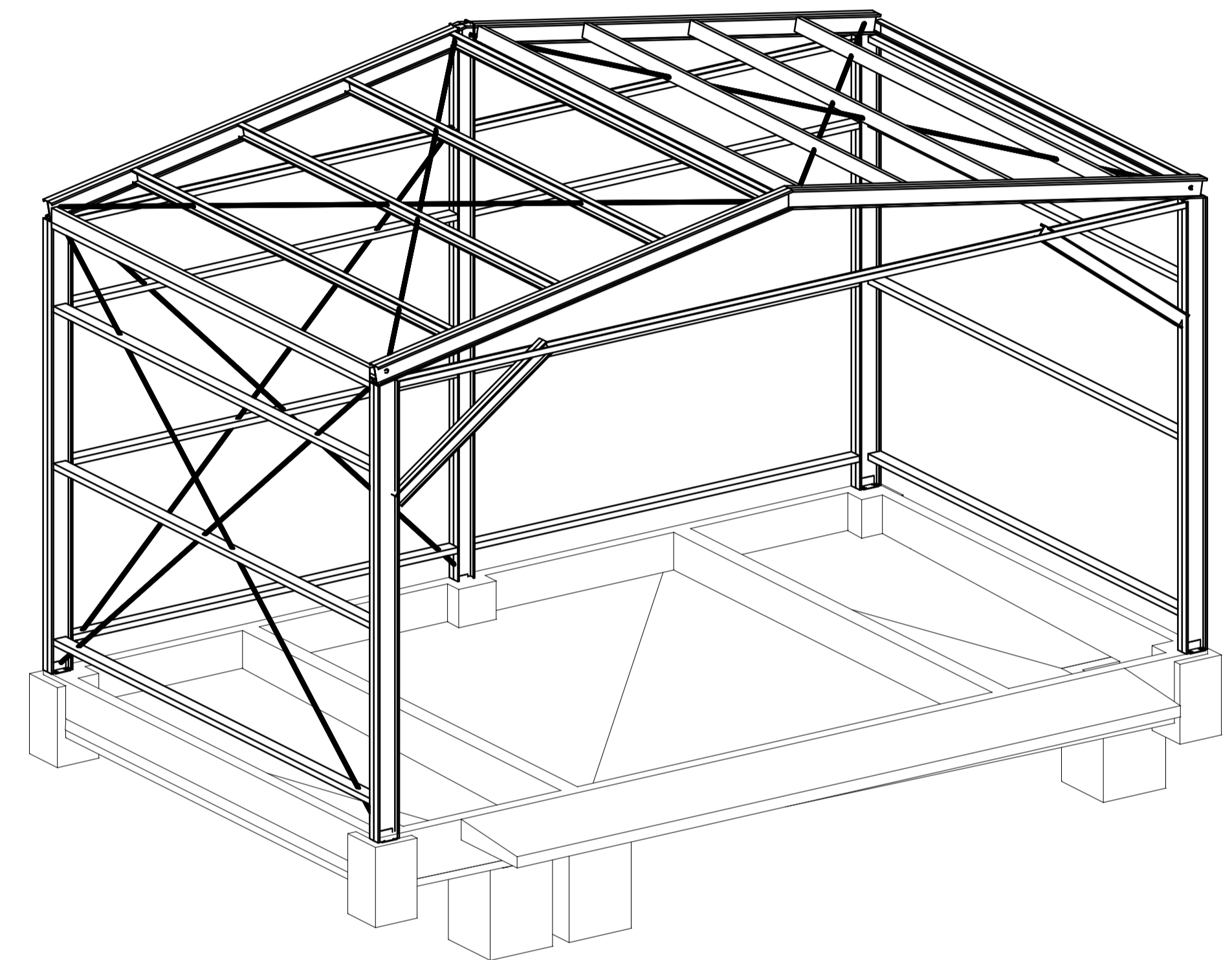
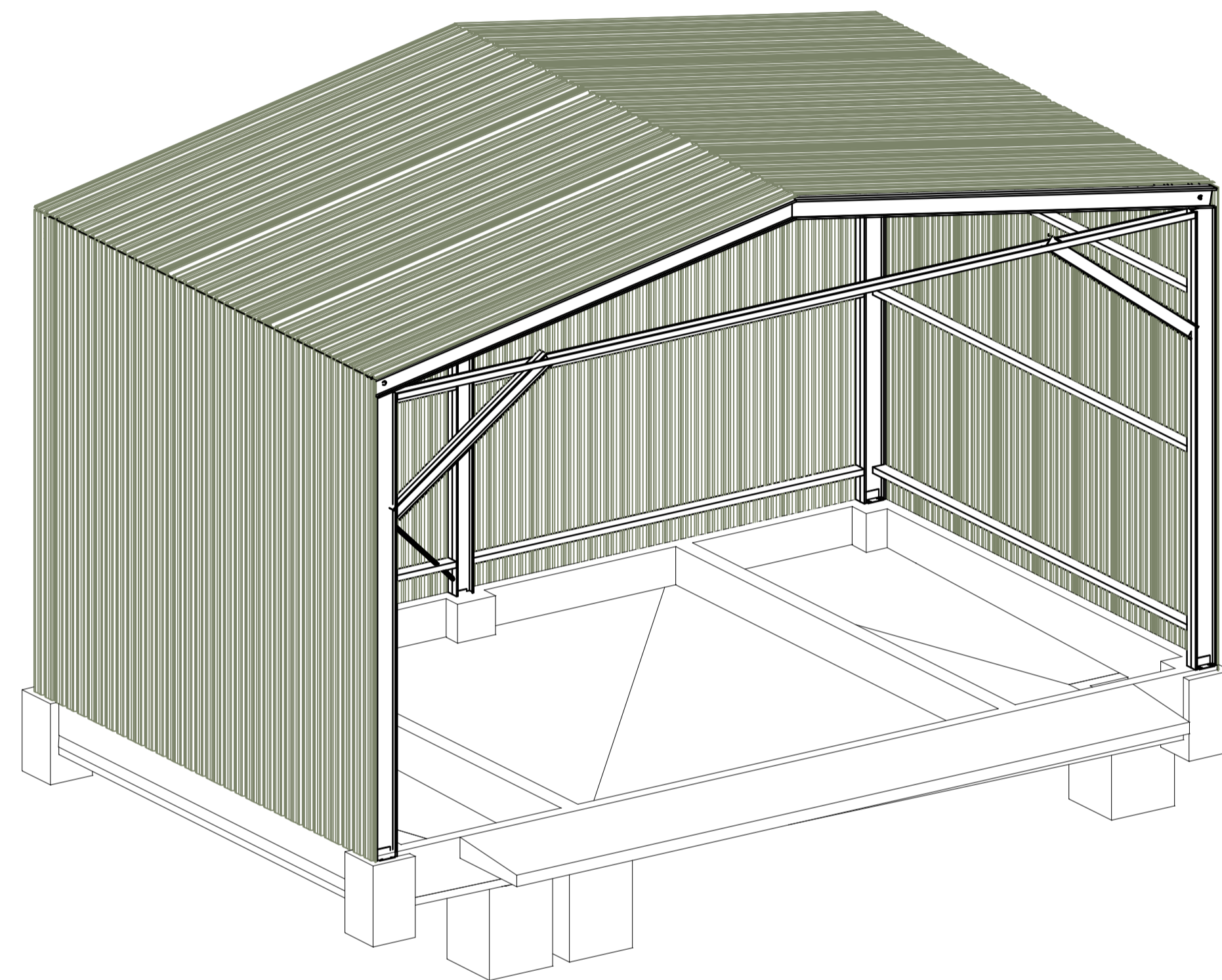


Figure 20 Reagents Storage Shed Isometric



AREA-1509- REAGENTS STORE AT WAREHOUSE - ISOMETRIC VIEW

ISSUED FOR APPROVAL
NOT FOR CONSTRUCTION



Plant and Infrastructure Engineering

DRAWN	JEL	20-04-21
CHECKED	KL B	20-04-21
DESIGNED	CPD	20-04-21
DES. APPR		
PROJ APPR		



CLIENT	Aurene Mt. Ida	SCALE	NTS	SIZE	A1
TITLE	MT. IDA GOLD PROJECT PLANT INFRASTRUCTURE LAYOUT	ALL DIMENSIONS IN MILLIMETRES			
AREA-1509- REAGENTS STORE AT WAREHOUSE - ISOMETRIC VIEW		REV No	0	DRAWING No	21007-1509-GEN-001

DRAWING No.	REFERENCE DRAWING TITLE	No	BY	DATE	REVISION DETAILS	CHKD	APPR	No	BY	DATE	REVISION DETAILS	CHKD	APPR	PROJ APPR

7.1.3 Carbon in Carbon in Pulp (CIP) Circuit

Works in the CIP area consist of the following:

- a) Seven (7) tanks make up the CIP circuit. Six (6) tanks are absorption tanks, and one (1) tank is the leach tank.
- b) Sodium Cyanide (NaCN) is used in the CIP Circuit requiring control and monitoring of cyanide levels. A cyanide analyser has been provided for this purpose.
- c) The CIP circuit is situated on a concrete floor with a bunded area equal to 110% of the largest tank. The bunded CIP circuit area can hold a volume of 1097kL and the largest tank in the CIP circuit has a volume of 893kL. The bunded area has a capacity of almost 123% of the largest CIP tank volume. **Photos 1, 2 and 3**
- d) Safety features to prevent personnel injury around the CIP circuit include handrails and suitable safety signs to warn of the danger from reagents and rotating equipment.
- e) Manually operated knife gate valves on the launders allow for offline tanks to be isolated.



Photo 7 CIP circuit bund – tailings thickener



Photo 8 CIP circuit bund – CIP vats



Photo 9 CIP circuit bund – CIP vats

7.1.4 Elution circuit

Works in the Elution and Gold Recovery area consist of the following:

- a) The Elution and Gold Recovery area includes two (2) vessels, the Acid Wash column and the Elution column. Both columns are certified pressure vessels situated in a structural steel

frame with steel columns fixed to concrete plinths on a concrete floor. There are safety valves fitted to the columns.

- b) Safety features to prevent personnel injury around the Elution and Gold Recovery circuit include handrails, overhead cranes and suitable safety signs to warn of the danger from reagents and equipment.

7.1.5 Surface water diversions

Not completed. Surface water diversions are part of the mining proposal non-process infrastructure and will be completed before the summer.

7.2 Process water pond

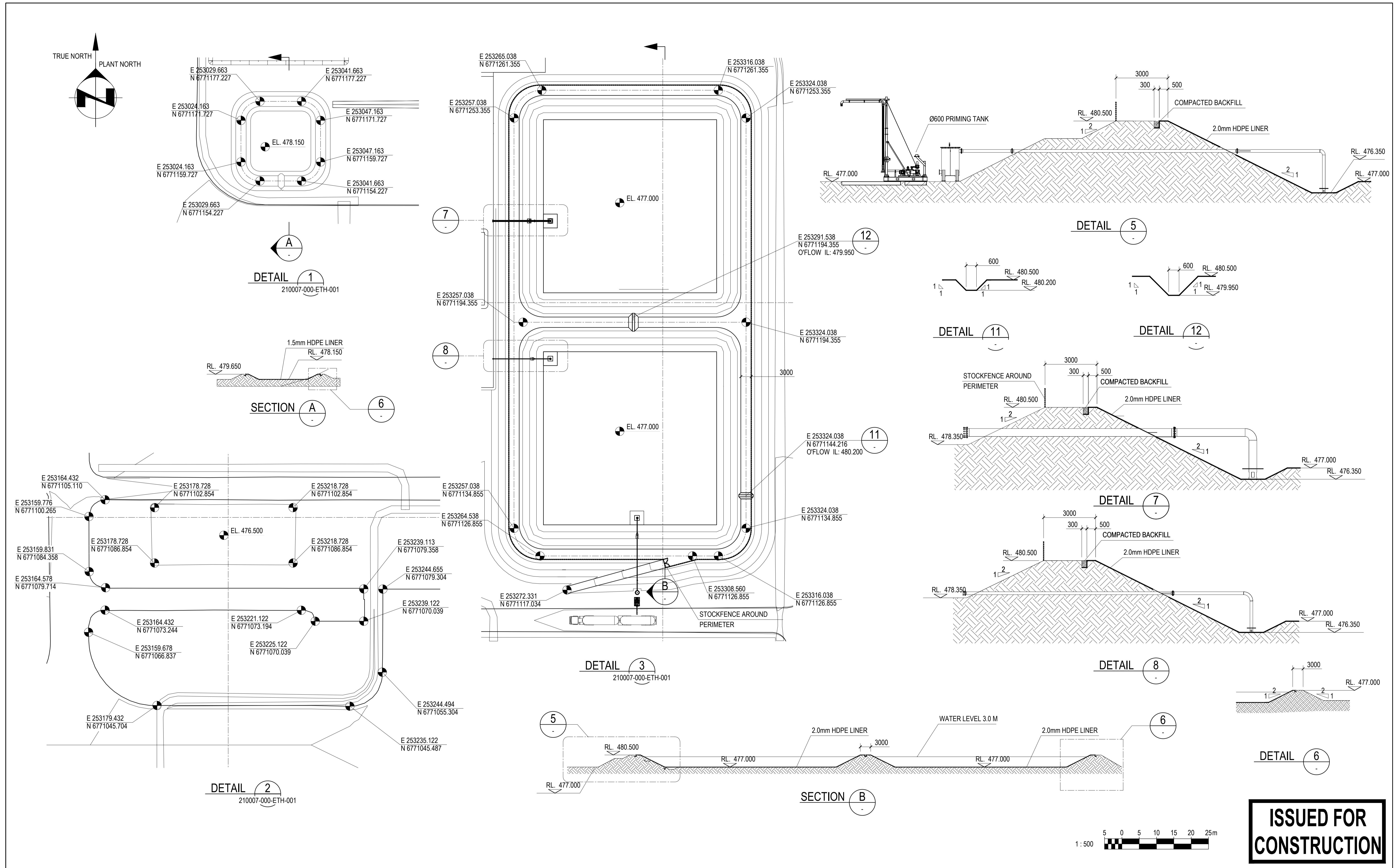
Works in the Process Water Pond area consist of the following:

- a) The Process Water Pond consists of an earth compacted wall 3.0m high. The wall is constructed to maintain a minimum of 300mm freeboard. (Designed freeboard is 500mm). The inner pond walls are lined with 2mm High Density Polyethylene (HDPE) having a permeability of not less than 1×10^{-9} m/s and are designed to contain a one in a hundred - year 72 hours ARI rainfall event (**Figure 21**)
- b) The Process Water Pond layout is in accordance with Figure 7 of Schedule 1 of the Works Approval.

7.3 Raw water pond

Works in the Process Water Pond area consist of the following:

- a) The Process Water Pond consists of an earth compacted backfill wall 3.0m high. The wall is constructed to maintain a minimum of 300mm freeboard. (Designed free board is 300mm).
- b) The inner pond walls are lined with 2mm High Density Polyethylene (HDPE) having a permeability of not less than 1×10^{-9} m/s are designed to contain a one in a hundred - year 72 hours ARI rainfall event (**Figure 21**)
- c) The Raw Water Pond layout is in accordance with Figure 7 of Schedule 1 of the Works Approval.



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DRAWING No.	REFERENCE DRAWING TITLE	No	BY	DATE	REVISION DETAILS	CHKD	APPR	No	BY	DATE	REVISION DETAILS	CHKD	APPR

DRAWN	JMC	21-06-21
CHECKED	KLB	21-06-21
DESIGNED	CPD	21-06-21
DES. APPR		
PROJ APPR		



CLIENT	Aurrene Mt. Ida
TITLE	MT. IDA GOLD PROJECT SITE EARTHWORKS ARRANGEMENT PLANT OVERALL EARTHWORKS LAYOUT

SCALE	1:500	SIZE	A1
ALL DIMENSIONS IN MILLIMETRES			
REV No	J 0		
DRAWING No	21007-0000-ETH-006		

Appendix A

PIE Engineering Report



Plant and Infrastructure Engineering

AURENNE MT IDA MT IDA GOLD PROJECT

REPORT ON DANGEROUS GOODS AND MINING APPROVAL COMPLIANCE

Report No
0104-RP-011

REV.	DATE	DESCRIPTION	AUTHOR	APPROVED
A	07/07/2023	<i>Issued for Comment</i>	[REDACTED]	

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APPENDIX 1 DRAWINGS

1 SCOPE

This report is a review of the compliance status for sections of the design, construction and installation of the Mount Ida Gold Project to meet the Mining Approval and Dangerous Goods requirements. The scope of this Report is based on Table 2 “Design and Construction/Installation Requirements” for the Process Plant, below. The sections covered are the Process Plant, Process and Raw Water Ponds and the Non-Process Infrastructure buildings and equipment in the process plant area.

Table 2: Design and construction/installation requirements

	Infrastructure	Design and construction requirements	Infrastructure location
1	Gold processing plant and associated infrastructure	<p>(a) Gold processing plant comprises the following infrastructure and equipment:</p> <ul style="list-style-type: none"> i. Run of mine (ROM) pad; ii. Crushing circuit – primary jaw crusher and secondary cone crusher; iii. SAG mill; iv. Carbon in pulp (CIP) circuit; and v. Elution and gold recovery circuit. <p>(b) Plant area to be constructed upon a concrete pad</p> <p>(c) Reagents, dangerous goods, and diesel to be stored in concrete bunded areas;</p> <p>(d) Carbon in Pulp (CIP) circuit to be located on a concrete floor and bunded with a capacity of 110% of the largest CIP tank;</p> <p>(e) Surface water diversions/sumps to be installed to divert stormwater away from operational areas; and</p> <p>(f) Layout of the processing plant to be in accordance with Figure 7 in Schedule 1.</p>	
2	Process water pond	<p>(a) HDPE lined (2.0 mm minimum) with a low permeability liner of 1×10^{-9} m/s and designed to contain a one in one hundred-year 72 hours ARI rainfall event;</p> <p>(b) Constructed to maintain a minimum 300 mm freeboard; and</p> <p>(c) Layout in accordance with Figure 7 of Schedule 1.</p>	
3	Raw water pond	<p>(a) HDPE lined (2.0 mm minimum) with a low permeability liner of 1×10^{-9} m/s;</p> <p>(b) Constructed to maintain a minimum 300 mm freeboard; and</p> <p>(c) Layout in accordance with Figure 7 of Schedule 1.</p>	

2 APPLICABLE DOCUMENTS

The scope of this Report relates to the current issue of documents listed below:

- a) W6640/2022/1 Works Approval – Department of Water and Environment
- b) Dangerous Goods Assessment Report and Risk Assessments – Mt Ida Gold Project – Aurene Mt Ida Pty Ltd

3 GOLD PROCESSING PLANT AND ASSOCIATED INFRASTRUCTURE

3.1 Run of Mine (ROM) Pad

Works on the ROM pad area consist of the following:

The ROM pad is a flat area approximately 120m by 120m in the shape of a 'U'. Windrows are situated along the lower half of the ROM pad 'U' to prevent or to arrest the haul trucks from running off the ROM pad.

3.2 Crushing Circuit

Works in the Crushing Circuit area consist of the following:

- a) Crushers, Conveyors, Surge Bin, Apron Feeder and an Emergency Stockpile. All this equipment was designed and installed to the relevant Australian Standards.
- b) The Crushing Circuit plant is constructed of structural steel with steel columns supported by concrete pads and plinths.
- c) Handrails, safety guards, and safety signs warning of dangers and hazards were placed in the appropriate areas to prevent or warn of potential injury.
- d) Lighting in the crushing circuit area is of sufficient brightness as to allow for easy operation of the plant during night shift operations.
- e) A lime bin is situated between the crushers and the Ball and SAG mills. A safety shower is situated next to the lime bin in case of an emergency.

3.3 Mills

Works in the SAG and Ball Mill area consist of the following:

- a) The SAG and Ball Mills are situated on engineer designed concrete pads and plinths.
- b) Safety features to prevent personnel injury around the SAG and Ball mills include handrails, guards and suitable safety signs.
- c) Electrical wiring and installations are protected from the environment. All electrical boxes are weatherproof and correctly identified with safety signs warning of any electrical danger.

3.4 Carbon in Pulp (CIP) Circuit

Works in the CIP area consist of the following:

- a) Seven (7) tanks make up the CIP circuit. Six (6) tanks are absorption tanks, and one (1) tank is the leach tank.
- b) Sodium Cyanide (NaCN) is used in the CIP Circuit requiring control and monitoring of cyanide levels. A cyanide analyser has been provided for this purpose.
- c) The CIP circuit is situated on a concrete floor with a bunded area equal to 110% of the largest tank. The bunded CIP circuit area can hold a volume of 1097kL and the largest tank in the CIP circuit has a volume of 893kL. The bunded area has a capacity of almost 123% of the largest CIP tank volume.
- d) Safety features to prevent personnel injury around the CIP circuit include handrails and suitable safety signs to warn of the danger from reagents and rotating equipment.
- e) Manually operated knife gate valves on the launders allow for offline tanks to be isolated.

3.5 Elution and Gold Recovery Circuit

Works in the Elution and Gold Recovery area consist of the following:

- a) The Elution and Gold Recovery area includes two (2) vessels, the Acid Wash column and the Elution column. Both columns are certified pressure vessels situated in a structural steel frame with steel columns fixed to concrete plinths on a concrete floor. There are safety valves fitted to the columns.
- b) Safety features to prevent personnel injury around the Elution and Gold Recovery circuit include handrails, overhead cranes and suitable safety signs to warn of the danger from reagents and equipment.

- c) Safety showers have been installed in close proximity to these two columns, the goldroom and the electrowinning circuit.

3.6 Reagents

Works in the Reagents area consist of the following:

- a) The reagents stored on site are Quicklime (CaO), Sodium Hydroxide (NaOH), Cyanide (CN⁻), Hydrochloric Acid (HCl), Nitric Acid (HNO₃), Hypochlorite Solution (ClO⁻), Carbon (C), compressed Oxygen (O₂) and Flocculant. NaOH, HCl and CN⁻ reagents are stored in the plant reagents area and consist of three (3) separately bunded tanks. Quicklime is stored in a silo for direct feed onto the mill feed conveyor.
- b) The Reagent Store has storage allocated for NaOH, HCl and HNO₃ in plastic totes for use in the laboratory, fresh Carbon in bulk bags and Flocculant in smaller bags. The acids and NaOH are stored in bunds separated by a 5 meter space where the Carbon and Flocculant are stored in the middle bund of the Reagent Store. The Reagent Store outer bund wall is 400mm high.
- c) ClO⁻ is stored in the Camp Reagent store in 200L drums under cover.
- d) HNO₃ and NaOH is used and stored in the Laboratory. Larger quantities of these reagents are stored outside on spill containment bunded pallets. The outside storage areas of HNO₃ and NaOH are more than 5 meters apart. Smaller quantities of laboratory reagents are stored inside in a DG cabinet.
- e) For safety reasons a 5 meter separation distance has been maintained between the Sodium Cyanide (NaCN) and Hydrochloric Acid (HCl) solutions. The NaOH, HCl and CN⁻ reagent storage tanks are contained within concrete bunds sized to contain 110% of the largest tank volume including from wall spray.
- f) Safety features to prevent personnel injury around the Reagents storage area include suitable safety signs to warn of the danger from reagents and safety showers.
- f) Bulk diesel is stored in self-bunded storage tanks. The unloading slab in front of the bulk storage is graded to drain to the waste oil sump. The heavy vehicle fuelling slab is drained to the heavy vehicle washdown facility which has an oily water separator. The power station day tank and waste oil tank are contained within concrete bunds.

3.7 Process Water Pond:

Works in the Process Water Pond area consist of the following:

- a) The Process Water Pond consists of an earth compacted wall 3.0m high. The wall is constructed to maintain a minimum of 300mm freeboard. (Designed freeboard is 500mm). The inner pond walls are lined with 2mm High Density Polyethylene (HDPE) having a permeability of not less than 1×10^{-9} m/s and are designed to contain a one in a hundred – year 72 hours ARI rainfall event.
- b) The Process Water Pond layout is in accordance with Figure 7 of Schedule 1 of the Works Approval.

3.8 Raw Water Pond:

Works in the Process Water Pond area consist of the following:

- a) The Process Water Pond consists of an earth compacted backfill wall 3.0m high. The wall is constructed to maintain a minimum of 300mm freeboard. (Designed freeboard is 300mm). The inner pond walls are lined with 2mm High Density Polyethylene (HDPE) having a permeability of not less than 1×10^{-9} m/s and are designed to contain a one in a hundred – year 72 hours ARI rainfall event.
- b) The Raw Water Pond layout is in accordance with Figure 7 of Schedule 1 of the Works Approval.

4 NON – PROCESS INFRASTRUCTURE AT THE PLANT

4.1 LNG Storage

Works in the LNG Storage area consist of the following:

- a) The position of the LNG Storage facility has not changed from the position noted in Figure 7: Process plant proposed layout of the mining approval. The orientation of the tanks has changed to meet safety exclusion requirements. Only one (1) LNG tank has been installed with the second tank scheduled for future works.
- b) Fire hydrants and fire hoses have been installed as per Drawing 21007-0000-PIP-GEN-001 Rev11.
- c) Safety signs have also been erected indicating entry restrictions and safety requirements for the LNG area.

4.2 HV / LV Workshop and HV Washdown Bay

Works in the HV / LV Workshop area consist of the following:

- a) The HV / LV Workshop has been moved approximately 130 meters west from its original site. The move was in response to environmental concerns. The orientation of the HV /LV Workshop has changed but all other aspects of the workshop remain the same.

The unchanged workshop items include the structural design and size of the workshop, the bunded area for the dispensing and storage of lubricants. A waste lubricant sump that incorporates a submersible pump for transferring the lubricant waste to the oil separator at the HV Washdown Bay.

The safety requirements and signs for the HV /LV Workshop have not changed and are as per the design.

- b) The HV Washdown Bay has been moved approximately 50 meters west and its orientation has been rotated by 90 degrees. All other aspects of the HV Washdown Bay remain unchanged. The oil separator removes the oil from the HV washdown water and other sources e.g. the HV/ LV Workshop, the Lubricant Store and the Power Station.

The oil removed by the oil separator is pumped to the waste oil tank. Water is reused by cleaning through a sand filter. Excess water is treated as oily water and sent to the Oily Water Pond where the water is evaporated off and the oily residue is collected and disposed of in accordance with environmental guidelines.

4.3 Lubricant Store

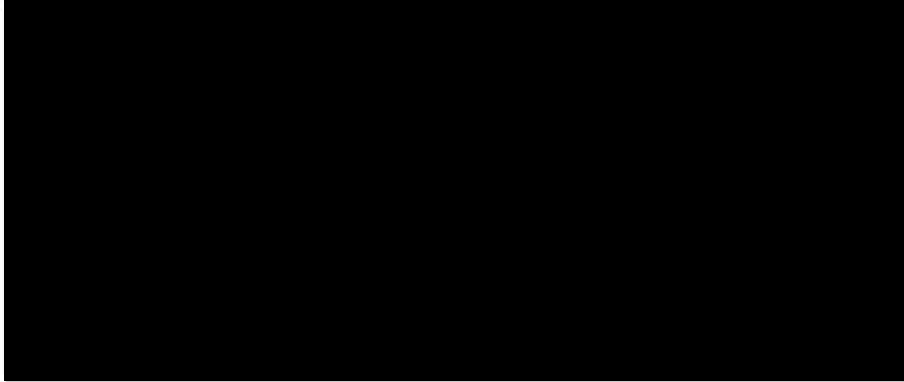
Works in the Lubricant Store area consist of the following:

- a) The Lubricant Store has been moved approximately 35 meters north so it can be covered by the nearest fire hydrant. The Lubricant store houses a range of lubricants and grease for the all the mining operations.
- b) A 400mm high bund wall encapsulates the Lubricant Store with a sump serviced by a submersible pump that delivers spilled lubricant to the HV Washdown Bay for separation by the oil separator for disposal.
- c) Safety and Hazard signs are displayed inside and outside of the Lubricant Store.

5 CERTIFICATION

5.1 Compliance with Design

As detailed above, PIE can certify that the works constructed to date meet the requirements of the Works Approval and Dangerous Goods compliance as required by the documentation.



APPENDIX 1 DRAWINGS

Drawings Process Plant

Drg. No.	Rev	Description
21007-0000-GEN-002	R	Figure 7 Works Approval, Mt. Ida Gold Project, Plant Infrastructure Layout, Overall General Arrangement
Aurenne Mining		Figure 1 Works Approval, Prescribed Premises Boundary
21007-000-ETH-006	C	Mt. Ida Gold Project, Site Earthworks Arrangement, Plant Overall Earthworks Layout (Process & Raw Water Ponds)
BCG 0100-L-002		Aurenne Alt Resources Pty Ltd, Mt. Ida Gold Project, General Plant Layout
Plant Layout 01		Isometric View of the Process Plant
Plant Layout 02		Isomeric View of the Process Plant
Plant Layout 03		Plan View of Process Plant and Non Process Infrastructure

Drawings Non-Process Infrastructure

Drg. No.	Rev	Description
21007-0000-PIP-GEN-001	11	Mt. Ida Gold Project, Utilities and Process Plant, Buried Services Layout 1 of 8
LNG-WA-082-G-01-A		Evol LNG, Mount Ida Gold Project, Evol LNG Facility, General Arrangement
LNG-WA-082-J-01-A		Evol LNG, Mount Ida Gold Project, Evol LNG Facility, Jet Fire Location
21007-1509-GEN-001	O	Mt. Ida Gold Project, Plant Infrastructure Layout, Area-1509 Reagents Store at Warehouse – Isometric View
21007-1509-GEN-002 Markup	PJ O	Mt. Ida Gold Project, Plant Infrastructure Layout, Area-1509 Reagents Store at Warehouse – Plan Layout
21007-1509-GEN-003	O	Mt. Ida Gold Project, Plant Infrastructure Layout, Area-1509 Reagents Store at Warehouse – Elevation Layout
21007-1510-GEN-001	C	Mt. Ida Gold Project, Plant Infrastructure Layout, Area-1510 Lube Store at Warehouse – Isometric View
21007-1510-GEN-002	C	Mt. Ida Gold Project, Plant Infrastructure Layout, Area-1510 Lube Store at Warehouse – Plan Layout
21007-1510-GEN-002	C	Mt. Ida Gold Project, Plant Infrastructure Layout, Area-1510 Lube Store at Warehouse – Elevation Layout

**AURENNE MT IDA
MT IDA GOLD PROJECT**

Drg. No.	Rev	Description
21007-1505-ARC-002	K	Mt. Ida Gold Project, Plant Infrastructure Layout, Area 1505 Laboratory Plan Layout
68454-ASM-001-C-GA2 Approved		Diesel Storage General Arrangement
21007-2670-GEN-003	E	Mt. Ida Gold Project, Plant Infrastructure Layout, Area 2670 – Diesel Storage Elevation Views
68454-DWG-001-B		Waste Oil Storage Tank

